

# **Photochimie du bâti : sources et puits de polluants oxydants (Acronyme: photoBAT)**

## **RECAPITULATIF DU PROJET**

**Titre du projet:** Photochimie du bâti : sources et puits de polluants oxydants  
(Acronyme: photoBAT)

**Thème de l'APR:** Thème I – Traceurs et parts attribuables

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## Rapport scientifique

### Avant propos.

Conformément à la convention signée, ce rapport présente l'ensemble des résultats scientifiques obtenus et est rédigé en anglais, utilisant les tirés à part de publications.

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## I. INTRODUCTION

Clean air is essential for people's health and for the quality of the environment. However, since the industrial revolution, the quality of the air that people breathe has deteriorated considerably - mainly as a result of human activities. Rising industrial and energy production, the burning of fossil fuels and the dramatic increase in traffic contribute to air pollution in our towns and cities which, in turn, can lead to serious health problems. For example, air pollution is increasingly being cited as the main cause of lung sickness such as asthma - twice as many people suffer from asthma today compared to 20 years ago.

Air pollution originating from traffic is an important problem in most urban areas. Nitrogen oxides ( $\text{NO}_x$ ), volatile organic compounds (VOCs) and particulate matter (PM) are some of these pollutants. Not only there are strong associations between ambient air pollution levels and adverse health effects<sup>1</sup> but also their transformation within the atmosphere leads to photochemical air pollution.<sup>2</sup> As a result, several regulations have been implemented to reduce emissions from vehicles and also a new approach has been applied in recent years by considering the use of self-cleaning and de-polluting materials to remove these pollutants.

The need to deliver cleaner air has been recognised for several decades with action having been taken at national and EU levels and also through active participation in international conventions. EU action has focused on establishing minimum quality standards for ambient air and tackling the problems of acid rain and ground level ozone. Polluting emissions from large combustion plants and mobile sources have been reduced; fuel quality improved and environmental protection requirements integrated into the transport and energy sectors.

Despite significant improvement, serious air pollution problems remain. Against this backdrop, the Community's Sixth Environmental Action Programme (6th EAP) called for the development of a thematic strategy on air pollution with the objective to attain "levels of air quality that do not give rise to significant negative impacts on, and risks to human health and the environment". Following its communication on the Clean Air For Europe programme (CAFE), the Commission has examined whether current legislation is sufficient to achieve the 6th EAP objectives by 2020. This analysis looked at future emissions and impacts on health and the environment and has used the best available scientific and health knowledge. This analysis showed that significant negative impacts will persist even with an effective implementation of current legislation.

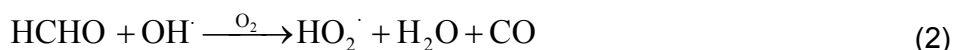
Among the new technical "solutions" designed for large dissemination over the public space, new building and coating materials are being widely proposed to stakeholders as well as public consumers.

Titanium oxide,  $\text{TiO}_2$ , has become the material of choice in a variety of remediation processes due to its photocatalytic properties<sup>3, 4</sup> and its favourable physical and chemical properties.<sup>3</sup> Besides, it is chemically inert in the dark, not expensive, non toxic and of easy handling. The self-cleaning properties of  $\text{TiO}_2$  are ruled by the absorption of band gap light and the production of excited-state conduction-band electrons and valence-band holes, which can react with electron acceptors and electron donors adsorbed on the semiconductor surface.<sup>4</sup> The environmental relevance of  $\text{TiO}_2$  is usually related to its overall capacity to deplete organic pollutants from aqueous and gaseous media. Many studies have recently focused on the development of environmental friendly materials by adding  $\text{TiO}_2$  to ordinary building materials such as concrete or by preparing  $\text{TiO}_2$  film coatings<sup>5-9</sup>. Although various photocatalytic materials are already on the market, very little reliable information is available, except for limited technical data, regarding their impact on air quality considering the potential formation of harmful chemical intermediates. This scenario motivates further studies on the field.<sup>8</sup>

Different works were focused on achieving the removal of  $\text{NO}_x$  from air by means of de-polluting surfaces containing  $\text{TiO}_2$ <sup>5,9-22</sup>. However, recent studies showed that UV-illuminated surfaces of pure  $\text{TiO}_2$  aerosols can reduce  $\text{NO}_2$  to HONO, together with the production of  $\text{H}_2\text{O}_2$ .<sup>23,24</sup> Besides the important impact of nitrous acid (HONO) as a free radical source in the atmosphere,<sup>25</sup> there are several mechanisms by which HONO may be harmful for health. Firstly, HONO is an

acid, which may damage mucous membranes and surfaces of the respiratory tract. Secondly, in the reaction of HONO with amino groups of the nucleotides, the double helix of the DNA can be cross-linked<sup>26-30</sup> leading to mutagenic properties. In addition, in the reaction of HONO with amines, both in the atmosphere but also in-vivo, nitrosamines are formed<sup>31-34</sup> which show carcinogenic and mutagenic properties.<sup>35,36</sup> Langridge *et al.* have recently reported the formation of nitrous acid on a self-cleaning window glass coated by TiO<sub>2</sub>.<sup>37</sup> As well, the photo-enhanced NO<sub>2</sub> uptake for real mineral dusts with HONO production was assigned to the chemistry occurring on the TiO<sub>2</sub>.<sup>38,39</sup> In this process, nitrate anions are formed as a consequence of the photocatalytic oxidation of NO<sub>2</sub> on UV-illuminated TiO<sub>2</sub> surfaces.<sup>14,23,40-43</sup> Most of these studies argue that nitrate is the innocuous final product of the photocatalytic NO<sub>x</sub> removal process. However, the photochemistry of nitrate doped mineral dust samples containing TiO<sub>2</sub> was proved to be a potential renoxification process of the atmosphere.<sup>44</sup> As well, the photochemistry of adsorbed nitrate on aluminium oxide has been proved to give different yields of NO, NO<sub>2</sub> and N<sub>2</sub>O according to the presence of water and molecular oxygen.<sup>45,46</sup>

Formaldehyde (HCHO) is an important and highly reactive compound present in all regions of the atmosphere, arising from the oxidation of biogenic and anthropogenic hydrocarbons. HCHO is a key compound in tropospheric chemistry. It is a strong HO<sub>x</sub> source (through its photolysis) and is therefore strongly connected to regional O<sub>3</sub> production. The main HCHO removal processes from the atmosphere are currently thought to be its photolysis and the reaction with OH according to<sup>47</sup>:



These removal processes are homogeneous and will happen throughout the troposphere. However, it is known that HCHO is chemically taken up, in the atmosphere, by sulphuric acid aerosols<sup>48</sup>. Therefore, one may question if similar heterogeneous reactions may occur on other surfaces such as mineral surfaces or buildings.

In this project, we studied the efficiency of these photocatalytic materials for air pollution reduction in the urban environment. In the very recent years, photo-catalytic self-cleaning and “de-polluting” materials have been suggested as a remediation technology mainly for NO<sub>x</sub> and aromatic VOCs in the polluted urban environment. The associated technologies have been launched on the European market with the aim to have a positive impact on urban air quality. These commercial products are based on the photo-catalytic properties of a thin layer of TiO<sub>2</sub> deposited at the surface of the material (such as glass, pavement, ...) or embedded in paints or concrete. The use of TiO<sub>2</sub> photocatalysts as an emerging air pollution control technology has been reported in many European areas. However, it seems that both the effectiveness and the real impact on air quality of these relatively new technologies up to now have been demonstrated only in a very limited manner before going into the European market.

Assessing the effectiveness of these depolluting techniques have a real added value both in terms of policy making (and implementing the EU air quality strategy) and economics (by providing a demonstration of the actual performance of a new technique).

This project aims at evaluating the feasibility of using TiO<sub>2</sub> based products to alleviate the air pollution problem under real atmospheric conditions.

We studied the degradation of nitrogen dioxide and formaldehyde, both key players in urban air pollution, on different substrates containing TiO<sub>2</sub> using dedicated flowtube techniques and atmospheric simulation chambers.

**In the next sections we will describe these experimental layouts and show that:**

- Nitrogen oxides are efficiently degraded on these photocatalytic surfaces
- Nitrous acid is produced in variable yields, depending on many parameters including surface pH (HONO release may be observed from alkaline surfaces such as cement based products)

The reactivity of NO<sub>2</sub> on irradiated TiO<sub>2</sub> / SiO<sub>2</sub> films was studied, with different TiO<sub>2</sub> contents, as proxies for NO<sub>x</sub> de-polluting materials. The influence of the photocatalyst concentration, the role of molecular oxygen and the effect of nitrate

on the reactivity of TiO<sub>2</sub> films were investigated. NO, HONO and nitrate anions are produced as a consequence of the NO<sub>2</sub> loss on UV-illuminated TiO<sub>2</sub> films. A renoxification pathway that involves the photochemistry of the NO<sub>3</sub> radical leads to the release of NO, NO<sub>2</sub> and of HONO from the TiO<sub>2</sub> surface. The presence of O<sub>2</sub> in the carrier gas modifies the NO and HONO production yields in the heterogeneous reaction between NO<sub>2</sub> and TiO<sub>2</sub> as well as the products of the renoxification process.

- Formaldehyde is also efficiently degraded on these photocatalytic surfaces.

The kinetics of the heterogeneous reaction between gaseous HCHO and TiO<sub>2</sub>/SiO<sub>2</sub> mineral coatings have been investigated to mimic HCHO loss on TiO<sub>2</sub> coated depolluting urban surfaces, by means of flow tube studies. The measured uptake kinetics were observed to be strongly enhanced when the surface (or coating) was irradiated in the wavelength range from 340 to 420 nm (with an irradiance of 1.45 mW cm<sup>-2</sup>). The associated BET uptake coefficient were measured in the range from  $(3.00 \pm 0.45) \times 10^{-9}$  to  $(2.26 \pm 0.34) \times 10^{-6}$  and were strongly dependent on the HCHO initial concentration in the range 3.5 - 32.5 ppbv, relative humidity from 6 to 70%, temperature from 278 to 303 K and TiO<sub>2</sub> content in the mineral coating from 1 to 100% wt. The measured kinetic was well described using a Langmuir-Hinshelwood type formalism. The estimated uptake coefficients were used to discuss the importance of the heterogeneous HCHO surface loss, in terms of deposition lifetimes, as compared to major homogeneous gas phase losses (OH reaction and photolysis). It is found that deposition may compete with gas phase removal of HCHO in a dense urban environment if more than 10% of urban surface is covered with TiO<sub>2</sub> treated materials.

- TiO<sub>2</sub> coating of urban surfaces may significantly affect the smog production chemical cycles  
The atmospheric degradation of propene in the presence of NO<sub>x</sub> has been investigated under atmospheric conditions in the presence and absence of materials that contain TiO<sub>2</sub>. The experiments have been conducted in different types of atmospheric simulation chambers using lamps and sun as the light sources (indoor and outdoor). The data obtained show that the presence of the TiO<sub>2</sub>-doped materials used in this work does have an impact on the chemical processes occurring during the oxidation of propene under atmospheric conditions. Comparison between the concentration profiles of the chemical species (C<sub>3</sub>H<sub>6</sub>, NO, NO<sub>2</sub> and O<sub>3</sub>) versus photolysis time in the presence and absence of the TiO<sub>2</sub> containing materials show that the consumption of propene is enhanced in the presence of TiO<sub>2</sub> with a larger consumption after a time delay. The enhancement seems to occur once the NO<sub>2</sub> maximum concentration is observed. The obtained results are discussed in terms of the possible atmospheric impact of these chemical processes on air quality.

## II. EXPERIMENTAL

### II.a Mineral oxides: Preparation and characterization

Experiments were performed with different mass mixing ratios of mineral oxides, in the range from 1 to 100 wt%, by diluting titanium dioxide TiO<sub>2</sub> (Degussa-P25, 80% anatase, 20% rutile; P25) in silica SiO<sub>2</sub> (Degussa Aerosil 130). All mixtures were prepared by suspending a total 3 g in 30 mL of ultra pure water (Aquadem milli-Q50). A few milliliters of these sonicated suspensions were dripped uniformly into dried Pyrex tubes (20 cm × 1.1 cm i.d) used as insert for the kinetic measurements (see below), rotated and dried at 373 K. The resulting film covered the entire inner surface of the tube and, to the eye, was fairly uniform in thickness.

However, the knowledge of the film morphology is of great importance for interpreting gas uptake processes. Therefore, scanning electron microscopy (SEM) coupled to Energy Dispersive X-ray spectroscopy (EDX) was used for the characterization of the dried film. For this purpose, the Pyrex inserts were cut in 1 cm long samples (considering finally only both ends and middle parts of the tube), dipped vertically into a mould holding an epoxy resin (araldite epoxy CY 230-ESCIL) and an epoxy resin hardener (HY 956-ESCIL) in a ratio (resin/hardener) equal to 2.5. After 12 hours, the mixture dried and hardened, was forming a polymer at room temperature. The polymer section (holding the tubes inserts) was then polished (ESC 200 GTL polisher from ESCIL) for a better image resolution. Finally, these SEM samples were coated with a thin layer of gold to enable electrons conduction to the observed area. Films at different TiO<sub>2</sub> mixing ratios (1, 5, 50 and 100% wt) have been observed. In addition, the analysis of different zones confirmed the uniformity of the film all along the tube for each sample. Films thickness ranged from 20 to 30 μm. Figure 1 displays both the SEM image of a TiO<sub>2</sub>/SiO<sub>2</sub> coating (50wt %) (Part a) and the surface profile of an area scanned from 0 (the Pyrex surface) to 40 μm (polymer matrix) (Part b). It is clear that the film sticks strongly to the Pyrex surface, fitting with any surface defect (see Figure 1.a). Besides, the EDX detection of the yellow line scanned in Figure 1.a corroborates with the film's chemical composition. Indeed, when the probe scanning runs from the Pyrex surface to the polymer matrix, two successive silicon peaks appear. They can be ascribed to the Pyrex composition (higher peak) and to the coating (lower peak). As expected, the titanium peak appears at 11 μm probe scanning and extends on 24 μm (i.e. the film thickness). It reaches the concentration of the lower silicon peak since both TiO<sub>2</sub> and SiO<sub>2</sub> are equally distributed in the film (TiO<sub>2</sub> 50%wt / SiO<sub>2</sub> 50%wt coating). Note that the Ti and Si concentrations are estimated to 15% wt of the coating as the gold deposited at the SEM sample is also detected. The cartography of another 50%wt TiO<sub>2</sub> sample scanned from the Pyrex glass tube (right) to the film (left) (shown with a 4000 magnification in Figure 1c) proves that the Ti and Si atoms are equally and homogeneously distributed in a 50% TiO<sub>2</sub> film.

### II.b Minerals for Chamber studies (ICARE and LISA)

The non treated glass is a standard window glass while the treated glass is a Pilkington™ Activ© self cleaning glass. As comparison of results obtained from complementary chambers as the basis of our strategy, all samples used among the consortium were from the same type and producer. Moreover, experiments were conducted using glass from the same production lot. The conditioning procedure was homogenized among partners consisting in a washing procedure based in a full rinsing with ultra pure water.

### II.c Experimental set-up

#### II.c.1 Flow Reactor

The uptake experiments were conducted in a horizontal cylindrical coated-wall flow tube reactor made of Pyrex. The Pyrex tube containing the TiO<sub>2</sub>/SiO<sub>2</sub> film was placed in the reactor, which was surrounded by 3 fluorescent lamps (OSRAM Sylvania TLD15W/08) having a continuous emission in the 340–420 nm range with a total irradiance of  $1.5 \times 10^{15}$  photons cm<sup>2</sup> s<sup>-1</sup>. NO<sub>2</sub> was introduced in

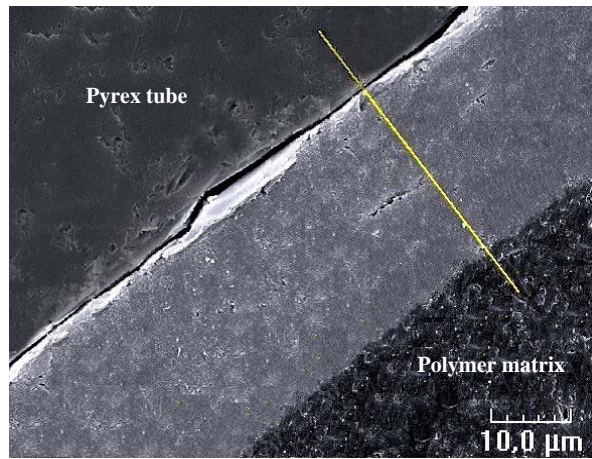
the flow tube by means of a movable injector with radius 0.3 cm. Synthetic air as well as pure nitrogen were used as carrier gases with a total flow rate of 200 sccm in the flow tube reactor, ensuring a laminar regime. The NO<sub>2</sub> and NO concentrations were measured at the reactor exit as a function of the injector position along the tube. This position determined the exposure time of the film surface towards the gas. A THERMO 42C chemiluminescent analyzer was used for NO and NO<sub>2</sub> detection. The latter is based on the reaction between NO and O<sub>3</sub>, which produces a characteristic luminescence with an intensity that is linearly proportional to the NO concentration. NO<sub>2</sub> is transformed into NO by means of a molybdenum converter in order to be measured with the chemiluminescent reaction. As HONO is detected by the same instrument as NO<sub>2</sub>, a denuder tube (9 cm × 0.95 cm i.d.) containing a mixture of K<sub>2</sub>CO<sub>3</sub> / Na<sub>2</sub>CO<sub>3</sub> (Fluka) was introduced between the exit of the flow cell reactor and the detector. The denuder was either bypassed, leading to the detection of NO and NO<sub>2</sub> together with HONO; or it was switched into the sample line along the experiment, so that only NO and NO<sub>2</sub> species were measured after HONO removal from the gas stream. Therefore, HONO concentration was obtained as the difference of the detector signal without and with the carbonate denuder in the sampling line.<sup>49</sup>

Gas phase NO<sub>2</sub> concentration used in the experiments was fixed in 150 ppbv ( $3.8 \times 10^{12}$  molec cm<sup>-3</sup>). The experiments were conducted at  $298 \pm 1$  K by circulating temperature-controlled water through the outer jacket of the flow tube reactor and were performed under atmospheric pressure and 30% of relative humidity. The temperature of the gas streams and the humidity were measured by using an SP UFT75 sensor (Partners BV). All gases were taken directly from cylinders without further purification prior to use. High purity synthetic air (99.999%), N<sub>2</sub> (99.0%) and NO<sub>2</sub> (1 ppmv in N<sub>2</sub>; 99.0%) were purchased from Air Liquide. The gas flows were monitored before entering the reactor by mass flow controllers (Brooks).

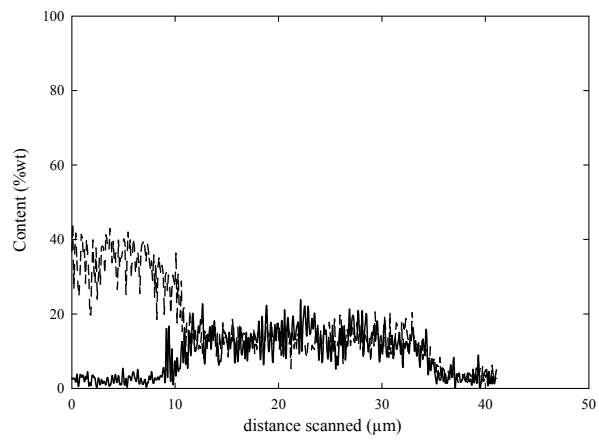
Periodical calibrations of the NO<sub>2</sub> from the cylinder were performed using the carbonate denuder. Only 3% of the total NO<sub>2</sub> (and possible contaminants) was trapped in the denuder, this value was then considered in the calculation of the uptake coefficients and products yield.

NO<sub>2</sub> may photodissociate with unit quantum yield in the wavelength region emitted by the lamps (300-420nm), but its loss in the gas phase is negligible for the residence time of 6 seconds used in our experiments. An estimation of the photolysis rate constant,  $J = 6.52 \times 10^{-4}$  s<sup>-1</sup> gives rise to a loss of 0.4% of the total NO<sub>2</sub> (g). Control experiments were performed to confirm the chemical inactivity of the Pyrex flow tube surfaces, and to evaluate the contribution of NO<sub>2</sub> photolysis. The empty tube (with no film) was filled with NO<sub>2</sub> and exposed to light. NO<sub>2</sub> photodissociation and loss at the Pyrex surface were negligible (below 3% of the total NO<sub>2</sub> loss) in comparison to the NO<sub>2</sub> loss observed in the presence of the TiO<sub>2</sub> / SiO<sub>2</sub> film.

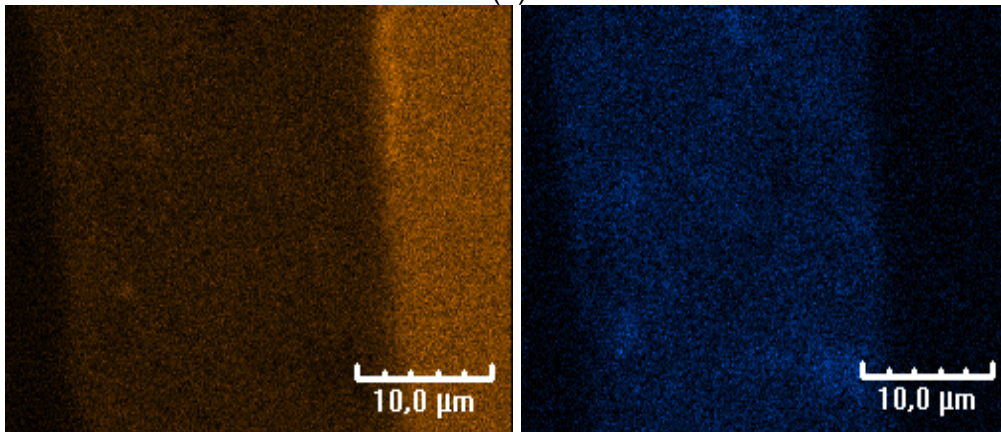
Gaseous formaldehyde was swept out from the reactor with Nitrogen from a home-made silicon permeation tube immersed in a 3.7 wt% HCHO solution at 298 K. The resulting gas mixtures were monitored at the reactor outlet with a portable HCHO analyzer fully developed at IRCELYON<sup>50</sup>. The relative humidity released from this permeation source of HCHO is ca. 6%. Formaldehyde is stripped out of the gas flow via a glass tube sampler, followed by a derivatization with 3-methyl-2-benzothiazolinone hydrazone (MBTH) in two successive steps in order to form a strongly absorbing chromophore<sup>51</sup>. The detection, in solution, of the converted HCHO was realized by means of a combination of a spectrograph (Andor technology / Shamrock SR - 163 i) coupled to a CCD camera (Andor Technology / iDus DV-420). Teflon AF2400 tubing (Biogeneral) were used as UV-visible long path cell<sup>52</sup>. Combining the strongly absorbing chromophore with a 100 cm long optical path led to a detection limit of ca. 3 pptv with 15 to 30 minutes resolution time depending on the first step conversion time. These formaldehyde measurements were validated against optical and chromatographic methods. Calibrations with Differential Optical Absorption Spectroscopy (DOAS) and Fourier Transformer Infrared spectroscopy (FTIR) showed less than 6% deviation. Similar results were obtained comparing to HCHO measurements by means of liquid chromatography coupled to UV-DAD detection subsequent to DNPH titration whether with Sepack cartridges<sup>53</sup> or with Radiello passive tubes trapping techniques<sup>54</sup>.



(a)



(b)



(c)

Figure 1: (a) SEM image showing the interface of 50%wt  $\text{TiO}_2 / \text{SiO}_2$  coating, (b) Surface profile of the yellow line scanned in part (a) displaying Ti (full line) and Si (dashed-line) concentrations (c) Cartography of another 50%wt  $\text{TiO}_2$  coating showing Ti (blue) and Si (yellow) distribution in the film.



## II.c.2 Uptake coefficient

The kinetic behaviour of the heterogeneous reaction between NO<sub>2</sub> and TiO<sub>2</sub>/SiO<sub>2</sub> films under irradiation can be well described by assuming a pseudo first-order reaction with respect to the gas-phase NO<sub>2</sub> concentration. The derived first-order rate constant,  $k_{\text{obs}}$ , is related to the geometric uptake coefficient ( $\gamma_g$ ) by:

$$\frac{d}{dt} \ln \frac{C_0}{C_i} = k_{\text{obs}} = \frac{\gamma_g \langle c_{\text{NO}_2} \rangle}{2r_{\text{tube}}} \quad (3)$$

where  $r_{\text{tube}}$ ,  $\gamma_g$ ,  $t$ , and  $\langle c_{\text{NO}_2} \rangle$  are the flow-tube radius (0.547 cm), the geometric uptake coefficient, the exposure time, and the NO<sub>2</sub> average molecular velocity, respectively.  $C_0$  is the NO<sub>2</sub> concentration when there is no contact between the film and the reagent; whereas  $C_i$  is the trace gas concentration when the contact with NO<sub>2</sub> is allowed. The uptake coefficient is defined as the fraction of effective collisions between a gas phase reagent and a reactive surface that lead to the loss of the gas phase reagent due to chemical reaction.  $\gamma_g$  is a mass dependent parameter for these substrates as diffusions and reaction of the trace gas take place at the internal surface of the films.<sup>41</sup> For that reason, a mass-independent uptake was derived by taking into account the entire BET surface area of the TiO<sub>2</sub>/SiO<sub>2</sub> films<sup>38,55</sup>.

Equation (3) does not contemplate possible diffusion limitations caused by the formation of a radial concentration gradient in the gas phase, which would occur if the loss at the surface is too fast to be recovered with the reagent supply. As a consequence, the uptake coefficient was calculated by using the Cooney-Kim-Davis (CKD) method<sup>56</sup>, which takes into account axial and lateral diffusion combined with a first order loss at the inner surface of a cylindrical tube under laminar flow conditions. An implementation of this method has been previously used.<sup>57</sup> The diffusion coefficient  $D$  was calculated using the formula proposed by Fuller *et al.*<sup>58</sup>

## II.c.3 CESAM chamber (LISA)

The experiments were carried out using a new Multiphase Atmospheric Experimental Simulation Chamber (CESAM, Figure 2) which has been constructed at LISA laboratory.<sup>59</sup> It consists of a 4.2 m<sup>3</sup> stainless steel vessel which can be roughly described as a vertical cylinder in which 6 glass plates (120 cm × 40 cm) are vertically hung offering a geometrical surface of 2.88 m<sup>2</sup>. A set of stainless steel magnetic torque mixing fans are installed inside the chamber reactor which allows to mix the gas phase compounds in less than 100 s. The chamber is equipped with a powerful solar simulator system which comprises 3 Xenon arc lamps of 4 kW each. This set-up provides an irradiation inside the chamber very close to the sun spectrum at the ground level (Figure 3). The lamps are symmetrically located above the chamber on a rigid framework. By optimizing the focal point of the light beam, it is possible to obtain a converging or diverging light beam with a maximum intensity inside the reactor; meanwhile the light spots projected at bottom level are as large as possible for minimizing the local overheating effects.

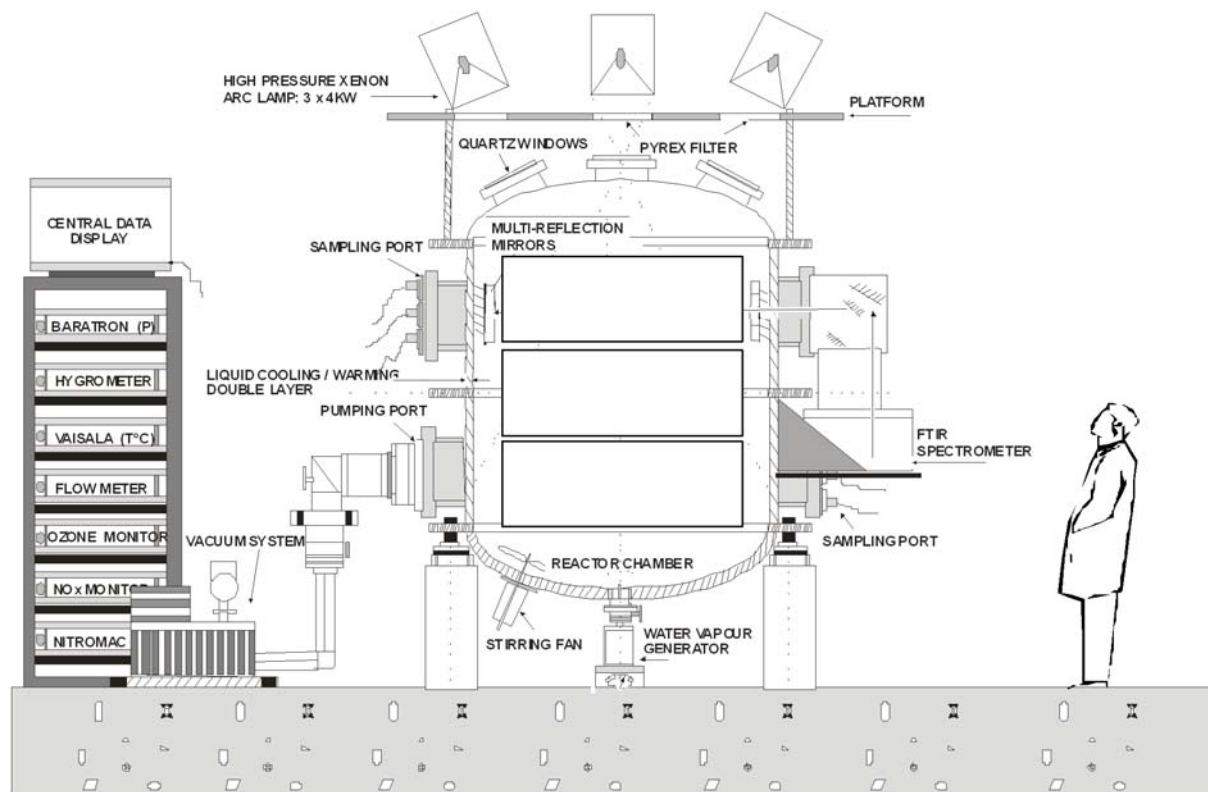
The photolysis frequency of NO<sub>2</sub> may vary in CESAM chamber by several physical parameters, such as the modifications of the Xenon lamps position and the irradiation sources aging.  $J_{\text{NO}_2}$  is thereby quantified periodically in the chamber before carrying out any experiment. For this study,  $J_{\text{NO}_2}$  was determined directly by measuring the actinic flux in the chamber (using a spectroradiometer LICOR LI1800) and indirectly by simulating the NO<sub>x</sub>/air/light chemical system during dedicated experiments<sup>60-61</sup>. The chemical actinometry determination of  $J_{\text{NO}_2}$  in CESAM chamber is described in detail by Wang *et al.*, 2010.  $J_{\text{NO}_2}$  can be calculated experimentally by considering the equation arising from the photostationary state hypothesis<sup>62</sup>,

$$J_{\text{NO}_2} = k_{(\text{NO}+\text{O}_3)} [\text{NO}][\text{O}_3]/[\text{NO}_2]$$

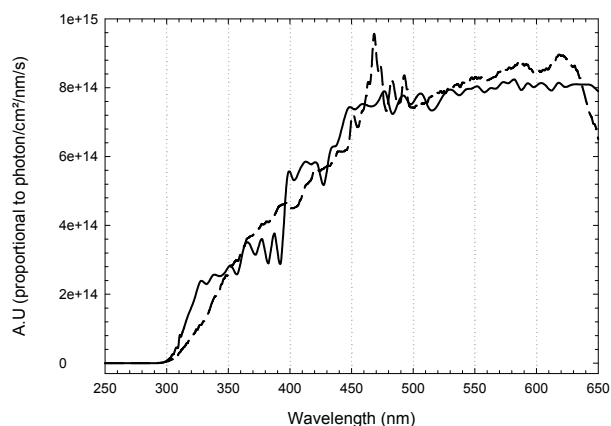
or determined by adjusting the observation curves and the numeric models (Wang, J.; Doussin, J. F. *et al.*, 2010). The obtained values for  $J_{\text{NO}_2}$  and  $J_{\text{O}(1D)}$  were respectively found equal to  $(3.5 \pm 0.5) \times 10^{-3} \text{ s}^{-1}$  and  $(1.2 \pm 0.2) \times 10^{-5} \text{ s}^{-1}$  in CESAM which is roughly one third of those measured in the boundary layer on a sunny day at mid latitude, in June at noon.

The chamber was evacuated to 10<sup>-4</sup> mbar before each experiment. Synthetic air was produced from the mixture of ca. 200 mbar of O<sub>2</sub> (AIRLIQUIDE, ALPHAGAZ<sup>TM</sup> class 1) and ca. 800 mbar of N<sub>2</sub> produced from the evaporation of a pressurized liquid N<sub>2</sub> tank. NO was purchased from

AIRLIQUIDE (ALPHAGAZ™ purity Class 2 UN1956). Experiments were carried out at atmospheric pressure and a temperature of  $293 \pm 2$  K. The simulation chamber is equipped with in-situ long path FTIR system (192 m) and with environmental analyzer. A Horiba™ APOA® 370 monitor was used for O<sub>3</sub> detection by means of a cross flow modulated ultraviolet absorption method while NO<sub>x</sub> measurements were performed using a Horiba™ APNA® chemiluminescence monitor. Nitrous acid was quantified using the NitroMac instrument<sup>63</sup> with a detection limit of 3 ppt for a time period of 10 minutes. Several experiments were performed in the absence of glass, in the presence of non treated surfaces and with TiO<sub>2</sub> treated surfaces inside the chamber. NO initial concentration ranged from 20 to 100 ppb and relative humidity was varied from 0 to 40%.



**Figure 2.** Scheme of the CESAM reactor. The three rectangles in bold represent the 6 plates of material set back to back in the chamber.



**Figure 3** Comparison of irradiation spectra. The thin black curve is the solar spectrum calculated from TUV NCAR, 12h, 45°N, 21 June. The dashed line curve is the spectra taken from inside the chamber with a Li1800 LICOR spectroradiometer.

#### II.c.4 Outdoor smog chamber with natural irradiation (ICARE)

The newly built Teflon chamber of 3.4 m<sup>3</sup> volume (Figure S4) was installed on the roof of the laboratory (ICARE – Orléans) for natural irradiation exposure. The chemical analysis were performed using commercial monitors (O<sub>3</sub>, NO, NO<sub>2</sub> and NO<sub>x</sub>). The physical parameters (pressure, temperature, relative humidity, light intensity (J<sub>NO2</sub>)) were continuously monitored using specific captors. In particular, J<sub>NO2</sub> was continuously measured using a 4 pi-sr J<sub>NO2</sub> filter radiometer (from meteorology consult GmbH) positioned inside the chamber. J<sub>NO2</sub> typical values were in the range (0.5-1)×10<sup>-2</sup> s<sup>-1</sup>. The ratio  $k_{(NO+O_3)} [O_3][NO] / J_{NO_2} [NO_2]$  was calculated using J values and NO, NO<sub>2</sub> and O<sub>3</sub> concentrations. For experiments conducted in absence of TiO<sub>2</sub> coated glass the ratio was 1, as predicted by the Leighton relationship. However, deviations from that value were observed when a TiO<sub>2</sub> coated glass was placed inside the chamber, indicating the occurrence of other efficient chemical processes.

A Teflon fan inside the chamber ensures the homogenisation of the gas mixture in less than 1 minute. Along the experiment, a slight air stream flowing into the chamber enables to compensate the sampling volumes and maintains a slight overpressure to prevent any possible contamination from outside air. A series of tests has been performed on the setup to ensure its reliability, such as leaks and homogenisation tests. The experiments were performed in the temperature range 293-301 K with a variation of 7 to 8 °C over the course of the runs. Several experiments were performed with the empty chamber, with non treated glass surfaces inside the chamber and in the presence of glass surfaces treated with TiO<sub>2</sub>. The relative humidity was maintained below 5%.

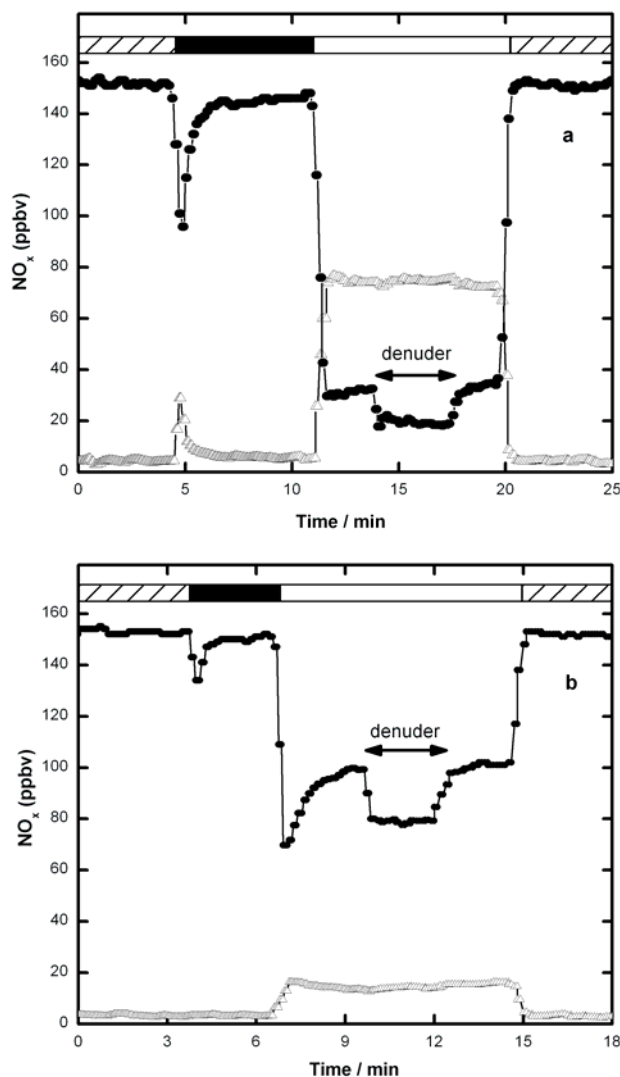


**Figure 4.** Picture of the ICARE outdoor chamber used in this work.

### III. RESULTS

#### III.1 Nitrogen Oxides

Figure 5 illustrates the behaviour of  $\text{TiO}_2$  (10%) /  $\text{SiO}_2$  films exposed to a continuous flow of 150 ppbv of  $\text{NO}_2$  in the dark and under irradiation for a fixed length of the flow tube. Figures 1a and 1b show the results obtained in pure  $\text{N}_2$  and in the mixture of  $\text{O}_2$  and  $\text{N}_2$ , respectively.



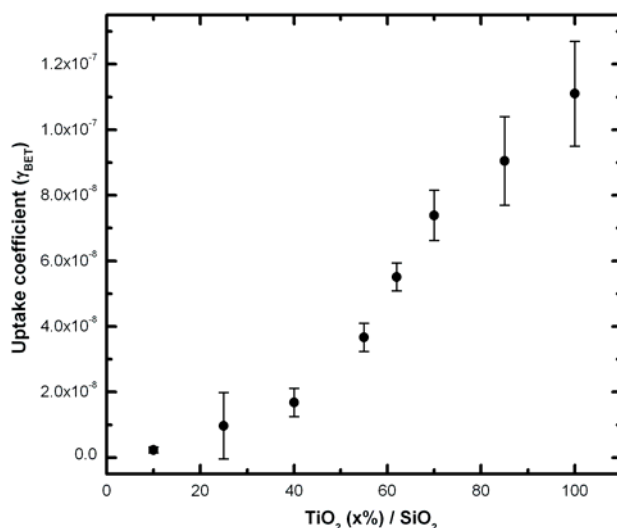
**Figure 5:**  $\text{NO}_2$  loss under irradiation of a  $\text{TiO}_2$  (10%) /  $\text{SiO}_2$  film when (a) only  $\text{N}_2$  was used as carrier gas, and (b) when the mixture  $\text{O}_2$  (15%);  $\text{N}_2$  (85%) was used as carrier gas. (●):  $\text{NO}_2$  signal; (△):  $\text{NO}$  signal. The dashed bars correspond to the initial concentration of  $\text{NO}_2$  which is not in contact with the film. The black and the white bars indicate the contact time between the  $\text{NO}_2$  flow and a certain length of the film in the dark and under irradiation, respectively. The inclusion of the denuder into the sample line is indicated in the figure (see Experimental).

A  $\text{NO}_2$  concentration of 150 ppbv was chosen for these studies because it can be found during intense photochemical pollution events in urban environments.<sup>23,64</sup> As well, it allowed varying the  $\text{TiO}_2$  content from 10 to 100% (as the observed rate is slower at higher gas phase concentrations). Once a constant initial  $\text{NO}_2$  concentration was established, the injector was withdrawn to a certain distance to expose some fraction of the film to  $\text{NO}_2$ , indicated in the top of the figure with a black bar. The  $\text{NO}_2$  was allowed to stabilize until it reached a *plateau*, before recovering the initial concentration with time. The uptake in the dark was more important in absence of  $\text{O}_2$  in the carrier gas for all residence times and for films with 10% and 100% of  $\text{TiO}_2$ . This behaviour may be related to the competition between  $\text{NO}_2$  and  $\text{O}_2$  for the adsorption sites on the film surface. When the lamps were turned on, a strong decrease of the  $\text{NO}_2$  signal was observed (it must be remembered that without the alkaline denuder this signal corresponds to the

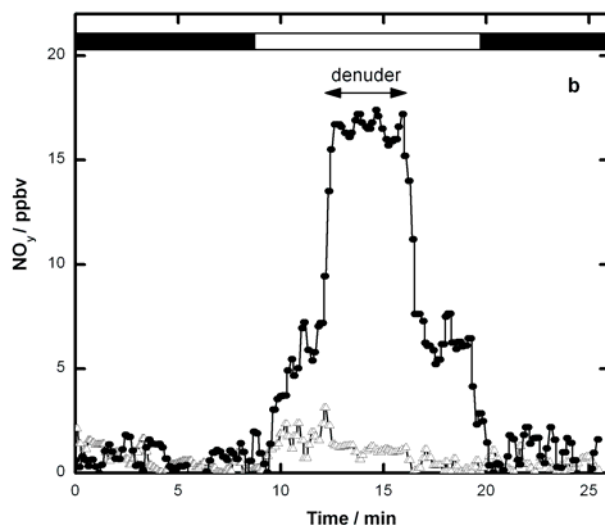
sum of the NO<sub>2</sub> and HONO species) highlighting a strong light induced uptake on these surfaces. The production of HONO was then verified under both conditions by passing the sample line through an alkaline denuder which trapped acidic species before detection. NO was produced both in absence and presence of O<sub>2</sub> in the carrier gas, the latter being in agreement with previous results.<sup>43</sup> When the lamps were turned off and the injector was moved forward to its original position, the initial NO<sub>2</sub> concentration was recovered. Figure 5 clearly shows that the NO<sub>2</sub> uptake on the samples as well as the NO and HONO formation were considerably enhanced under irradiation, both in presence and absence of molecular oxygen in the carrier gas for films with 10% wt. TiO<sub>2</sub>. The HONO yield was higher in presence of O<sub>2</sub> whereas the NO formation was favoured in the absence of O<sub>2</sub> (see Table 1).

**Table 1:** Effect of the carrier on the uptake coefficients, HONO and NO yields when exposing the films towards 150 ppbv of NO<sub>2</sub>. Errors are 2σ precision.

carrier	TiO <sub>2</sub> (x%)/SiO <sub>2</sub>	γ <sub>BET</sub>	HONO / %	NO / %
N <sub>2</sub>	10	(2.0 ± 0.6) × 10 <sup>-7</sup>	8 ± 2	50 ± 10
O <sub>2</sub> (15%) / N <sub>2</sub> (85%)	10	(2.2 ± 0.8) × 10 <sup>-9</sup>	14 ± 4	26 ± 8
N <sub>2</sub>	100	(1.5 ± 0.4) × 10 <sup>-6</sup>	3 ± 1	71 ± 8
O <sub>2</sub> (15%) / N <sub>2</sub> (85%)	100	(1.1 ± 0.2) × 10 <sup>-7</sup>	12 ± 4	-



**Figure 6:** Effect of TiO<sub>2</sub> content on the uptake coefficient when the films were exposed to 155 ppbv of gas phase NO<sub>2</sub> under irradiation using O<sub>2</sub> (15%) and N<sub>2</sub> (85%) as carrier. Error bars are 2σ precision.

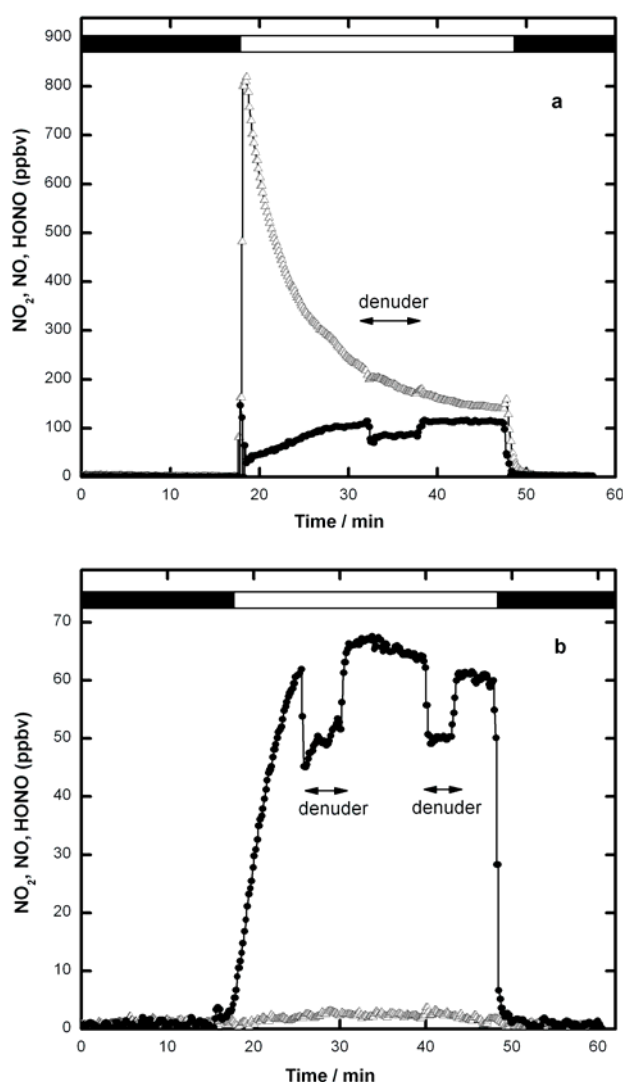


**Figure 7:** Effect of light on pure TiO<sub>2</sub> films which were previously exposed to NO<sub>2</sub> and light using: synthetic air as carrier gas. The black and the white bars indicate the contact time between the carrier flow and the total length of the film in the

dark and under irradiation, respectively. The inclusion of the denuder into the sample line is signalled in the figure. (●): NO<sub>2</sub> signal; (△): NO signal.

**Table 2:** Effect of the TiO<sub>2</sub> content on the gas phase product yields when exposing the films to 150 ppbv of NO<sub>2</sub> under irradiation. Errors are 2σ precision.

TiO <sub>2</sub> (x%)/SiO <sub>2</sub>	HONO / %	NO / %
10	14 ± 4	26 ± 8
25	35 ± 2	16 ± 4
40	28 ± 7	42 ± 9
55	36 ± 20	49 ± 20
62	11 ± 5	3 ± 1
70	10 ± 6	2 ± 1
85	27 ± 7	-
100	12 ± 4	-

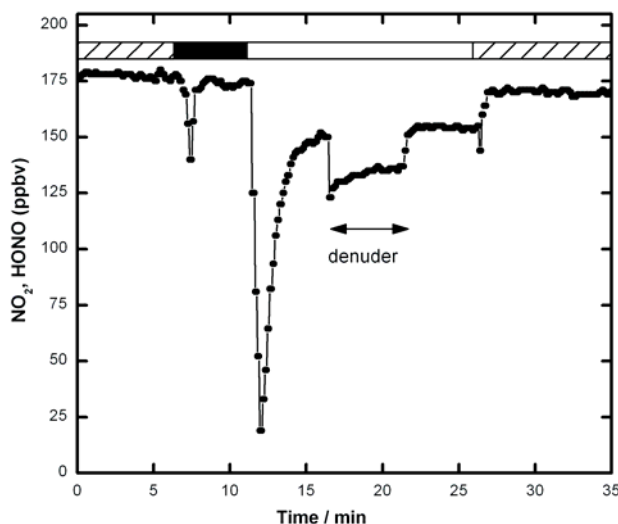


**Figure 8:** Effect of light on a TiO<sub>2</sub> / KNO<sub>3</sub> 50 % w film when (a): it is exposed to a flow of N<sub>2</sub>; and (b): it is exposed to a flow of synthetic air. The black and the white bars indicate the contact time between the carrier flow and the film in the dark and under irradiation, respectively. The inclusion of the denuder into the sample line is signalled in the figure. (●): NO<sub>2</sub> signal; (△): NO signal.

The effect of the TiO<sub>2</sub> content on the NO<sub>2</sub> loss was determined for illuminated TiO<sub>2</sub> / SiO<sub>2</sub> films (Figure 6). As it was expected, the uptake coefficients increased with increasing TiO<sub>2</sub> content

in the films, which *a priori* would indicate that the higher the content of TiO<sub>2</sub> at the surface, the more efficient it should be as a de-polluting material.<sup>5</sup> As shown in Table 2, HONO was produced for all TiO<sub>2</sub> concentrations tested under irradiation, while NO was produced only on films containing between 10 and 55 % of TiO<sub>2</sub>. Furthermore, the HONO + NO yields on the different TiO<sub>2</sub> / SiO<sub>2</sub> films were always lower than 100 %. This result may be explained by the formation of nitrate during the heterogeneous reaction between TiO<sub>2</sub> and NO<sub>2</sub> under irradiation.<sup>14,23,40-43</sup> Rodriguez *et al.*<sup>65</sup> have proved by photoemission data and DF (Density Functional) calculations that surface NO<sub>3</sub> is formed through the disproportionation of NO<sub>2</sub> on Ti sites.

After exposure to NO<sub>2</sub> under irradiation the films were flushed by a constant flow of synthetic air or pure N<sub>2</sub> (depending on the carrier gas used on each case) in order to promote molecules desorption from the surface. Once no further traces of NO and NO<sub>2</sub> were observed, lamps were turned on again and emission of different NO<sub>y</sub> species from the surface was observed. Figure 7 shows the formation of NO and NO<sub>2</sub> under irradiation for both carrier gases. In agreement with the results presented in Figure 5, NO was the major product in pure nitrogen (Figure 7a). However, not only NO<sub>2</sub> was the major product when air was used as carrier gas but also the production of another volatile compound was observed when passing the effluent flow through the carbonate denuder (Figure 7b). This product was observed for films which had previously been exposed to NO<sub>2</sub> under illumination and contained between 40 and 100% TiO<sub>2</sub>, and it was not observed when N<sub>2</sub> was used as carrier gas. We hypothesise that the signal observed switching the carbonate denuder into the sample line may be due to N<sub>2</sub>O formation, as previously observed by Rubasinghege and Grassian on aluminium oxide particle surfaces containing adsorbed nitrate.<sup>45</sup> These results may suggest that nitrate ions produced during the heterogeneous reaction of NO<sub>2</sub> and illuminated TiO<sub>2</sub> films may be involved in a renoxification process as previously discussed by Ndour *et al.* for mineral dusts containing TiO<sub>2</sub>.<sup>44</sup>



**Figure 9:** Effect of the NO<sub>2</sub> exposure under irradiation after the renoxification process on the same film of TiO<sub>2</sub> / KNO<sub>3</sub> 50 % w presented in Fig. 4b. The dashed bars correspond to the initial concentration of NO<sub>2</sub> which is not in contact with the film. The black and the white bars indicate the contact time between the NO<sub>2</sub> flow and the film in the dark and under irradiation, respectively. (●): NO<sub>2</sub> signal.

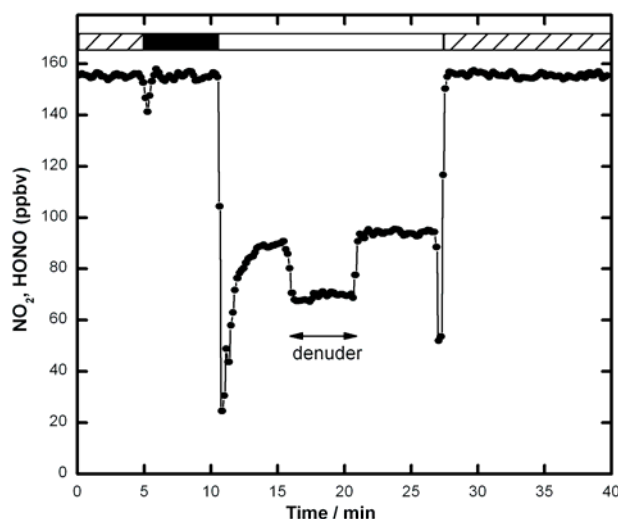
The proposed mechanism for the obtained gas phase products, which is consistent with that reported by Ohko *et al.*<sup>43</sup> is the following:

$\text{TiO}_2 + h\nu \rightarrow h_{\text{vb}}^+ + e_{\text{cb}}^-$	(4)
$\text{H}_2\text{O} + h_{\text{vb}}^+ \rightarrow \text{H}^+ + \text{HO}^\bullet$	(5)
$\text{NO}_2 + e^- \rightarrow \text{NO}_2^-$	(6)
$\text{NO}_2 + \text{HO}^\bullet \rightarrow \text{HNO}_3$	(7)
$\text{NO}_2^- + \text{H}^+ \rightarrow \text{HONO}$	(8)
$\text{NO}_2^- + h\nu \rightarrow \text{NO} + \text{O}^-$	(9)

In the presence of molecular oxygen, there is an electron transfer to O<sub>2</sub> that acts as the primary electron acceptor, leading to oxygen activated species<sup>4,66,67</sup> which can participate in the previous mechanism as follows:

$O_2 + e^- \rightarrow O_2^{\bullet -}$	(10)
$NO_2 + O_2^{\bullet -} \rightarrow NO_2^{\bullet -} + O_2$	(11)
$H^+ + O_2^{\bullet -} \rightarrow HO_2^{\bullet}$	(12)
$HO_2^{\bullet} + NO \rightarrow NO_2 + HO^{\bullet}$	(13)

These pathways explain the higher HONO yield and the lower NO yield obtained from the heterogeneous reaction between NO<sub>2</sub> and illuminated TiO<sub>2</sub> films in presence of O<sub>2</sub> in the carrier gas. The production of HO<sub>2</sub><sup>•</sup> by reaction (12) leads to the formation of H<sub>2</sub>O<sub>2</sub>, which has been observed by Beaumont *et al.*<sup>23</sup> Indeed, no H<sub>2</sub>O<sub>2</sub> is detected in absence of O<sub>2</sub>.<sup>4</sup> Gerischer and Heller<sup>68</sup> have suggested that electron transfer to O<sub>2</sub> may be the rate-limiting step in semiconductor photocatalysis. Hirakawa *et al.* have proved that O<sub>2</sub><sup>•-</sup> participates in the decomposition of alcohols.<sup>69</sup>



**Figure 10:** Effect of the NO<sub>2</sub> exposure under irradiation on a film of TiO<sub>2</sub> (55%) / SiO<sub>2</sub>. The dashed bars correspond to the initial concentration of NO<sub>2</sub> which is not in contact with the film. The black and the white bars indicate the contact time between the NO<sub>2</sub> flow and the film in the dark and under irradiation, respectively. (●): NO<sub>2</sub> signal.

A second set of experiments was performed to verify the role of nitrate anions in the renoxification process, using TiO<sub>2</sub> films prepared with 50 % wt of KNO<sub>3</sub>. Again, the role of molecular oxygen in the carrier gas was investigated. Figure 8a shows that NO was the major product when pure N<sub>2</sub> was used as carrier gas, in agreement with the results from Figure 7, while NO<sub>2</sub> and HONO were the main products in the presence of O<sub>2</sub> in the carrier gas. Similarly, Schuttlefield *et al.*<sup>46</sup> observed high NO<sub>2</sub> and low NO emission during the renoxification process of nitrate adsorbed on alumina surfaces in an atmosphere with oxygen. Rubasinghege and Grassian<sup>45</sup> suggested that oxygen vacancy sites may play a role in the photochemical process of adsorbed nitrate or on the chemistry of the photoproducts, as these sites may be binding sites for molecular O<sub>2</sub>. Figure 8 also shows that NO release in pure N<sub>2</sub> is faster than the release of NO<sub>2</sub> in air, which is also in agreement with the results shown in Figure 7. This difference can also be explained considering the affinity of O<sub>2</sub> for the adsorption sites of TiO<sub>2</sub>. Control experiments were carried out to determine whether nitrate photolysis was involved in the release of NO, HONO and NO<sub>2</sub>. None of these products were observed on films without TiO<sub>2</sub>; indeed irradiation of a SiO<sub>2</sub> / KNO<sub>3</sub> 50 % w and KNO<sub>3</sub> film did not lead to any NO<sub>y</sub> release; at least over our limit of detection. These control experiments indicate that nitrate photolysis was a negligible pathway in our experiments, in contrast with the mechanism proposed by Grassian and co-workers<sup>45,46</sup> on adsorbed nitrate on aluminium oxide particles. The proposed mechanism for the renoxification process has already been discussed by Ndour *et al.*<sup>44</sup> for dust samples irradiated in pure N<sub>2</sub>.

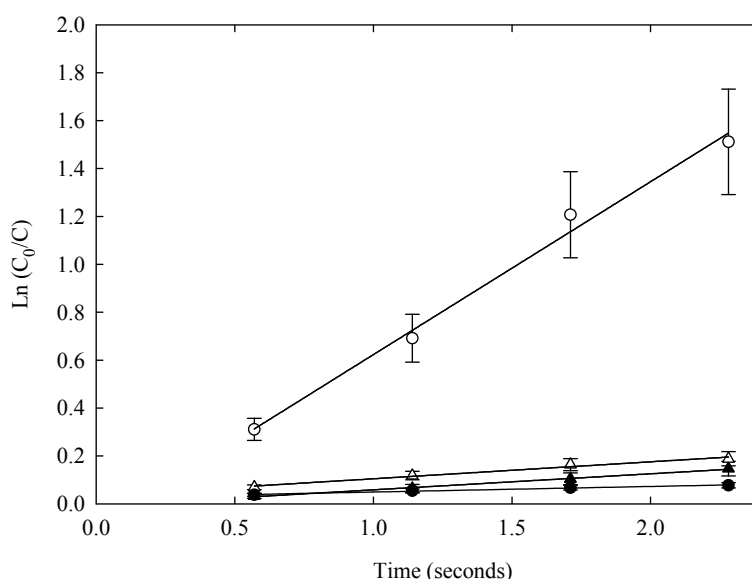


$\text{NO}_3^- + h\nu \rightarrow \text{NO}_3^*$	(12)
$\text{NO}_3^* + \text{O}_2 \rightarrow \text{NO} + \text{O}_2$	(13)
$\text{NO}_3^* + h\nu \rightarrow \text{NO}_2 + \text{O}$	(14)

The ability of a  $\text{TiO}_2$  /  $\text{KNO}_3$  50 %w film to remove  $\text{NO}_2$  (~170 ppbv) under irradiation in an atmosphere with  $\text{O}_2$  was also investigated. Figure 9 evidences that the  $\text{TiO}_2$  surface is active towards  $\text{NO}_2$  removal with HONO production under irradiation even when the film was prepared with a high content of nitrate. The observed  $\text{NO}_2$  loss (~35 ppbv) approximately balance the release of  $\text{NO}_2$  (~50 ppbv) from the renoxification process (Figure 8b) and the  $\text{NO}_2$  loss (~85 ppbv) observed on a film of  $\text{TiO}_2$  (55%) /  $\text{SiO}_2$  shown in Figure 10. These results are in disagreement with previous studies,<sup>42,43</sup> where the photocatalyst was deactivated by the nitrate ions produced during the photo-oxidation. But these previous investigations did not considered the renoxification process occurring at the surface of the  $\text{TiO}_2$  film when nitrate ions are deposited. This result suggests that HONO would not only be produced during the heterogeneous reaction between  $\text{NO}_2$  and a clean irradiated  $\text{TiO}_2$  surface but also on a  $\text{TiO}_2$  surface containing nitrate. As a consequence, special care should be taken in the development of an environmental friendly material which contains  $\text{TiO}_2$  in its matrix as undesired products may be also formed under irradiation.

### III.2 Formaldehyde

For all mineral coatings used in this study, the derived BET uptake coefficients measured in the dark were very low (of the order of  $3 \times 10^{-9}$ ). This indicates a weak loss of HCHO on the surface, which is, within our sensitivity, independent of the  $\text{TiO}_2/\text{SiO}_2$  mixing ratio. Similar to Carlos-Cueller et al (2003) we have observed low reactivity of HCHO onto  $\text{SiO}_2$  films.. Both dark and UV light conditions, led to uptake coefficients of ca.  $(3.1 \pm 0.5) \times 10^{-9}$  i.e., no photoenhancement was observed.



**Figure 11** Kinetic of logarithmic HCHO decay as a function of residence time for 11 ppb of HCHO, at 298 K at 6% of RH on different films mixing ratios. Circles and triangles correspond to measurements performed with pure  $\text{TiO}_2$  and pure  $\text{SiO}_2$  coatings respectively. Open and dark symbols are assigned to illuminated and dark conditions.

A very different behavior is observed for HCHO uptake onto  $\text{TiO}_2$  doped surface under illumination with weak near UV irradiation (irradiance of  $2.7 \times 10^{15}$  photons  $\text{cm}^{-2} \text{s}^{-1}$  in the 340-420 nm range). In this case the uptake is markedly photoenhanced (nearly 40 times greater than under dark conditions (see figure 11)). Under steady-state conditions, these findings underline the importance of the photocatalytic HCHO removal at the surface of the film containing traces of  $\text{TiO}_2$ . HCHO degradation by photocatalytic engineered systems was already described in the literature<sup>70-72</sup>. It is suggested that the photocatalytic oxidation of HCHO is due to surface reaction with OH radicals, produced by the reaction of the hole, created once  $\text{TiO}_2$  is irradiated with UV light, and

adsorbed water. However, to our knowledge there are no data available for the HCHO uptake coefficient on irradiated mineral dust films or proxy of them to be used for atmospheric purposes.

The irradiance used in this study, is approximately 5 times less than the solar irradiance between 340 and 420 nm reaching the Earth surface<sup>73</sup>. Therefore, we investigated the dependence of the BET steady-state uptake coefficient on the irradiance at 293 K, 30% RH and 2 ppbv of HCHO. As shown in Figure 12, the BET uptake coefficient is linearly dependent on the irradiance, which varied from  $1.9 \times 10^{15}$  to  $2.7 \times 10^{15}$  photons  $\text{cm}^{-2} \text{s}^{-1}$  confirming the heterogeneous photochemical nature of the HCHO loss. If the linearity observed in Figure 12 is extrapolated to the irradiance reaching the Earth ground in the same wavelength range at fixed HCHO mixing ratio and humidity, it is then possible to estimate an atmospherically relevant uptake coefficient. The BET uptake coefficients are normalized to the measured irradiance  $I$  reaching the film during the experimental determination, according to:

$$\Gamma_{\text{phot}} = \frac{\gamma_{\text{BET}}}{I} \quad (15)$$

where  $I$  is the irradiance reaching the film during the experimental determination. The obtained normalized coefficient,  $\Gamma_{\text{phot}}$ , has units of  $(\text{mW cm}^{-2})^{-1}$ . For the majority of the experiments,  $I$  was equal to  $1.45 \text{ mW cm}^{-2}$ . Then  $\Gamma_{\text{phot}}$  can be then multiplied by the irradiance reaching the Earth ground or the troposphere, making possible a rough assessment of the impact of light on the heterogeneous HCHO chemistry on  $\text{SiO}_2\text{-TiO}_2$  oxides; provided that all other parameters are kept constant.

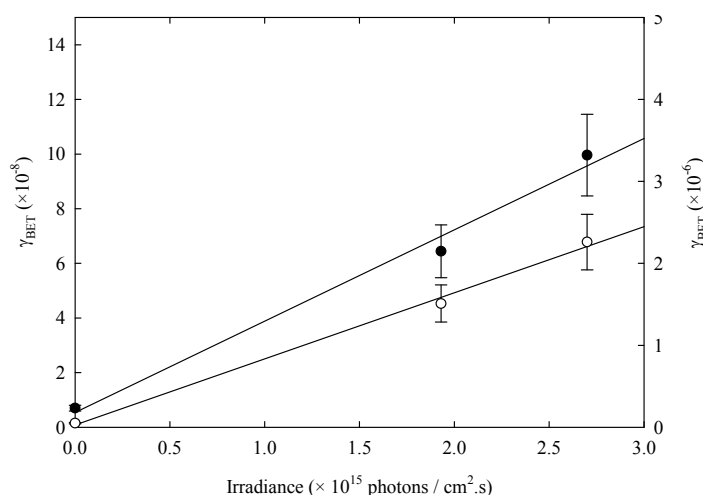


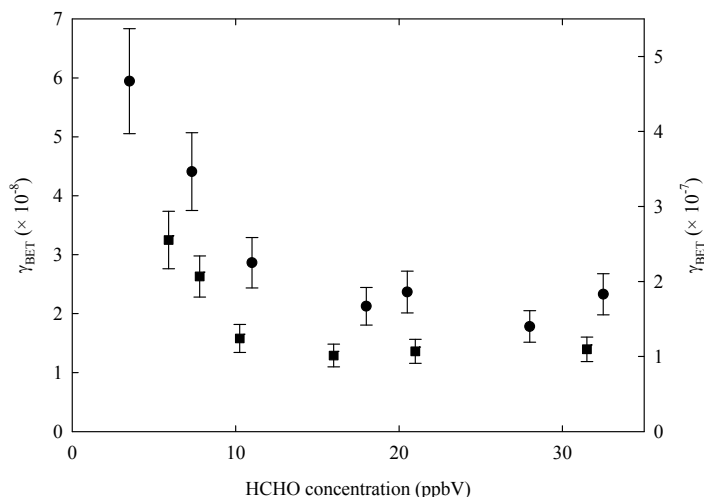
Figure 12: Dependence of the uptake coefficient as a function of UV light irradiance. Experiments were conducted with 2 ppbV of HCHO at 30% of RH and 293 K. Filled and open circles are raw data carried with 5% wt of  $\text{TiO}_2$  diluted in  $\text{SiO}_2$  and pure  $\text{TiO}_2$  coatings respectively. The latter data are related to the right hand scale.

Another important atmospheric variable parameter is the HCHO initial mixing ratio. The uptake coefficients were observed to be inversely dependent on the initial gaseous HCHO concentration. Figure 13 shows the uptake coefficient decreasing from  $(6.0 \pm 0.9) \times 10^{-7}$  to  $(2.0 \pm 0.3) \times 10^{-7}$  for pure  $\text{TiO}_2$  coatings and from  $(3.0 \pm 0.5) \times 10^{-8}$  to  $(1.5 \pm 0.2) \times 10^{-8}$  for 5%wt  $\text{TiO}_2$  films with increasing HCHO concentration in the range from 3.5 to 32.5 ppbv, with a plateau being attained around 10 ppbv. Our data clearly show that the rate is inversely proportional to the HCHO concentration, as previously observed in many heterogeneous studies onto different solid and liquid surfaces, both organic and inorganic<sup>74-79</sup>. More specifically, the inverse of the uptake rate has been observed to be dependent linearly with the inverse of the HCHO inlet concentration, in agreement with a Langmuir-Hinshelwood formalism.

The effect of water vapor on the uptake process was also investigated between 6 and 70% relative humidity (RH) for both 5 and 100%wt of  $\text{TiO}_2$ . As shown in Figure 14,  $\gamma_{\text{BET}}$  decreases at low (below 20%) and high humidity level (over 50-60%) and reaches a maximum at around 30% of RH. This, indicates that higher amount of water inhibits the surface loss. Such a dependence on the relative humidity has already been reported<sup>70,71,80,81</sup> and was explained by the competitive adsorption of water and the volatile organic compound (VOC) at the surface along with modifying

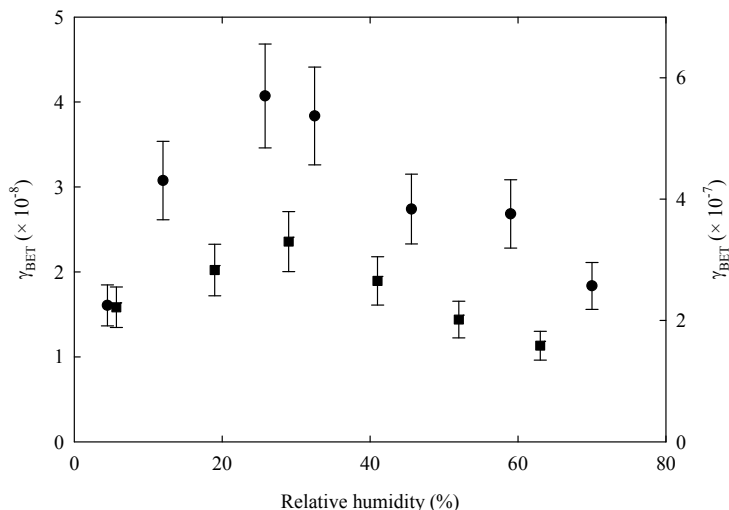
the amount of OH radicals produced at the TiO<sub>2</sub> surface, which is the driving force for the HCHO uptake. Similar conclusions certainly hold in the present study.

The results shown in Figure 15, indicate that the HCHO uptake coefficient increases from  $(1.8 \pm 0.3) \times 10^{-7}$  to  $(3.2 \pm 0.5) \times 10^{-7}$  for pure TiO<sub>2</sub> coatings and from  $(4.8 \pm 0.8) \times 10^{-9}$  to  $(2.0 \pm 0.3) \times 10^{-8}$  for SiO<sub>2</sub>/TiO<sub>2</sub> (5 %wt) with increasing temperature in the range from 278 to 298 K. As adsorption and chemical reactivity have opposite temperature trends, these observations indicate that the surface reaction controls the observed positive dependence on the temperature.



**Figure 13:** Trend of uptake coefficient as a function of the introduced HCHO concentration ranging from 3.5 to 32.5 ppbv. Experiments were performed with 6% of RH, at 293 K in UV-light conditions (lamps irradiance =  $2.7 \times 10^{15}$  photons cm<sup>-2</sup> s<sup>-1</sup>). Squares (■) and circles (●) correspond to measurements performed with 5% wt of TiO<sub>2</sub> diluted in SiO<sub>2</sub> and pure TiO<sub>2</sub> coatings respectively. The latter data are related to the right hand scale.

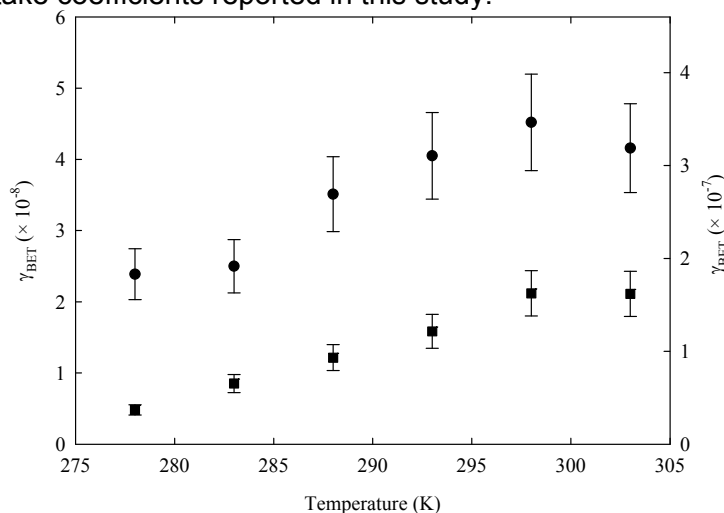
In the real environment, exposed surfaces may have variable TiO<sub>2</sub> content. We therefore tested mixing ratios between 1 and 100 wt % of TiO<sub>2</sub> in a SiO<sub>2</sub> matrix and the experimental results are presented in Figure 16, showing again a linear dependence of the uptake coefficient with respect to the wt % of TiO<sub>2</sub>.



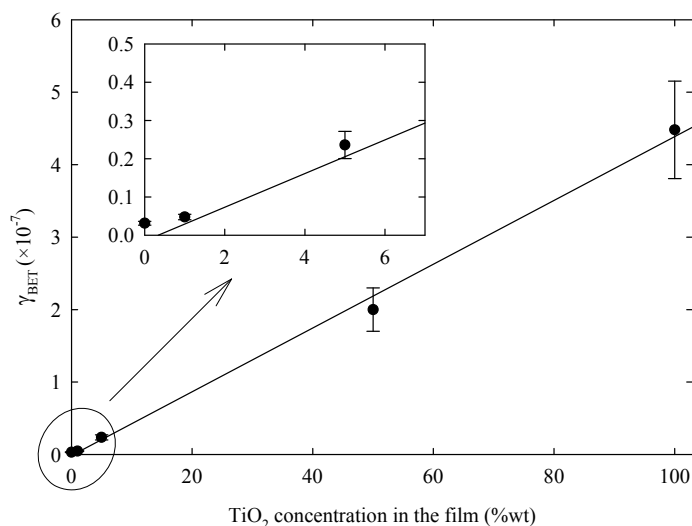
**Figure 14:** Effect of RH onto uptake coefficients. Experiments were carried out onto illuminated coatings with  $2.7 \times 10^{15}$  photons cm<sup>-2</sup> s<sup>-1</sup> and exposed to 11 ppb of HCHO at 293 K. Squares (■) and circles (●) correspond to measurements performed with 5% wt of TiO<sub>2</sub> diluted in SiO<sub>2</sub> and pure TiO<sub>2</sub> coatings respectively. The latter data are related to the right hand scale.

The present data show a strongly enhanced reactivity of synthetic surfaces containing TiO<sub>2</sub> and SiO<sub>2</sub>, taken as proxies for atmospheric dust particles when irradiated with weak near UV irradiation using a coated flow tube reactor. Under dark conditions, the steady-state uptake BET coefficient (determined after 30 min of HCHO exposure time to the surface) is estimated as  $(2.97 \pm 0.45) \times 10^{-9}$  onto SiO<sub>2</sub>/TiO<sub>2</sub> (5% wt) films and to  $(3.18 \pm 0.5) \times 10^{-9}$  onto pure TiO<sub>2</sub> coatings. Our results, compared to Xu et al. (2006) data conducted onto α-Al<sub>2</sub>O<sub>3</sub> particles at 293 K ( $\gamma_{\text{BET}} = (9.4 \pm 1.7) \times 10^{-9}$ ), are smaller<sup>82</sup>. Initial dark uptake kinetics of formaldehyde, onto pure mineral oxide

surfaces (i.e.  $\text{SiO}_2$ ,  $\alpha\text{-Fe}_2\text{O}_3$ ,  $\alpha\text{-Al}_2\text{O}_3$ ) measured by Grassian and co-workers at 295 K in a Knudsen-cell reactor operating at low pressure and under dry conditions<sup>83,84</sup> were showed to be much greater (in the range of  $3 \times 10^{-7}$  to  $1 \times 10^{-4}$ ) than our values (in the order of  $2 \times 10^{-6}$  for pure illuminated  $\text{TiO}_2$  coatings). One difference lies in the low time resolution of the present series compared with quasi instantaneous response in the molecular flow reactor. Another difference lies in the rapid surface deactivation they observed, in contrast to the sustained HCHO uptake for 3.5 hours exposure time measured in our work. Actually, water molecules and other trace gases can strongly interact with mineral oxide surfaces affecting the adsorption and reaction kinetics and so the HCHO uptake onto the surface. The photochemistry of mineral aerosols could be an important sink for HCHO in a dust plume. The global impact of such dust photochemistry is now facilitated by the photoinduced uptake coefficients reported in this study.



**Figure 15:** Effect of temperature on uptake coefficient. Experiments were driven with coatings illuminated with  $2.7 \times 10^{15}$  photons  $\text{cm}^{-2} \text{s}^{-1}$  and exposed to 11 ppb of HCHO at 30% of RH. Squares (■) and circles (●) correspond to measurements performed with 5% wt of  $\text{TiO}_2$  diluted in  $\text{SiO}_2$  and pure  $\text{TiO}_2$  coatings respectively. The latter data are related to the right hand scale.



**Figure 16:** Dependence of uptake coefficient with respect to  $\text{TiO}_2$  content in the coatings. Experiments were performed with coatings irradiated with  $2.7 \times 10^{15}$  photons  $\text{cm}^{-2} \text{s}^{-1}$  and exhibited to 11 ppb of HCHO at 30% of RH and at 293 K.

The dry deposition of HCHO is generally not suggested to be an efficient removal pathway. This has also been observed here as the HCHO uptake rate on pure  $\text{SiO}_2$  was very slow. However, adding  $\text{TiO}_2$  to construction materials may add a new removal pathway close to the ground. In fact, such materials, through the  $\text{TiO}_2$  photocatalytic properties, are suggested to be a sink for various organic pollutants. The kinetic information obtained in this study can be used to assess whether and under which conditions, HCHO removal through  $\text{TiO}_2$  based construction materials may be significant. For performing such an evaluation let us assume a city in which such materials are deployed at a large scale i.e., a city in which buildings are coated by a thin layer of  $\text{TiO}_2$  (as

already made in some locations). Let us assume that this TiO<sub>2</sub> layer covers between 0% (i.e., the case of most current cities) and 100% (a hypothetical futuristic case where all building are made with these TiO<sub>2</sub> based construction materials). Using previous modelling studies for dense urban areas<sup>85-87</sup>, which consider both the rates of occupied surface at the ground and shaped constructed surface, we estimate that the building surface exposed to HCHO deposition is 2.25 times the city surface at the ground. Current commercial TiO<sub>2</sub> based construction materials are covered by an approximately 10 nm thick active TiO<sub>2</sub> layer<sup>88</sup> having an internal (BET) surface as the films explored in this study. This would expose a total chemically active surface of  $1.04 \times 10^8$  m<sup>2</sup> taking into consideration a ground surface of  $46 \times 10^6$  m<sup>2</sup> (which would be Lyon's city surface<sup>89</sup>).

To assess if these processes may represent a significant HCHO sink, an easy way would be to compare the lifetimes associated to its main removal processes i.e., photolysis or reaction with OH to photoinduced uptake on the buildings. The first two lifetimes are readily available from the literature. Assuming an average OH concentration of  $10^6$  molecules cm<sup>-3</sup>, the OH channel lifetime is calculated to be almost 26 hours<sup>90</sup>. Considering a solar zenith angle of 30° and therefore an irradiance of  $1.92 \times 10^{17}$  photons cm<sup>-2</sup> s<sup>-1</sup><sup>91,92</sup>, HCHO is photolysed with a lifetime of 6 hours. The heterogeneous pathway (i.e., degradation at the surface of TiO<sub>2</sub> based construction materials) is evaluated by using the uptake coefficient derived in this study.

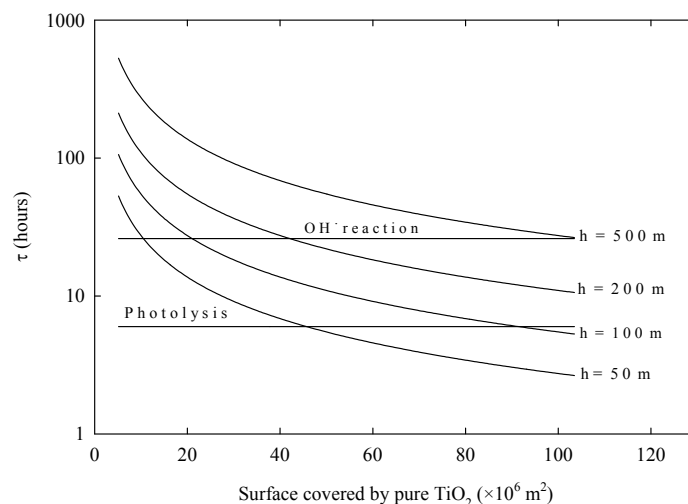
To a first approximation, equation (4) can still be used to calculate the HCHO lifetime just by replacing the volume of the tube by the volume of air in the urban environment (simply defined as the ground surface times the mixing height) and the surface by the total surface of photocatalytical active material deployed in this virtual city. For these calculations, we used the uptake coefficient measured at 2 ppbv at 30% relative humidity and 293 K linearly extrapolated to real solar conditions ( $I = 1.21 \times 10^{16}$  photons cm<sup>-2</sup> s<sup>-1</sup>) in the UV region (340 to 420 nm), we can estimate that, the associated uptake coefficient onto pure TiO<sub>2</sub> films, is  $(9.7 \pm 1.4) \times 10^{-6}$ .

Assuming a mixing height (h) between 50 and 500 m, the HCHO lifetime can be approximated to:

$$\tau_d(\text{hours}) = \frac{5.47 \times 10^6 \times h(\text{m})}{S(\text{m}^2)} \quad (16)$$

Figure 17 compares all three estimated lifetimes as a function of the urban TiO<sub>2</sub> coverage. Obviously, it can be seen that HCHO loss increases significantly from high to low mixing heights where the deposition process is forced. Compared to HCHO loss by means of OH reaction, deposition process onto urban surfaces from heights ranging from 100 to 200 m is significant if 20 and 40 % of constructed surface is covered by pure TiO<sub>2</sub>, respectively. Besides, we note that for the upper mixing heights, HCHO concentrations are estimated to be smaller which contribute, according to Figure 14, to faster kinetics deposition. In this case, one may reconsider uptake coefficients values in the calculation of HCHO lifetime.

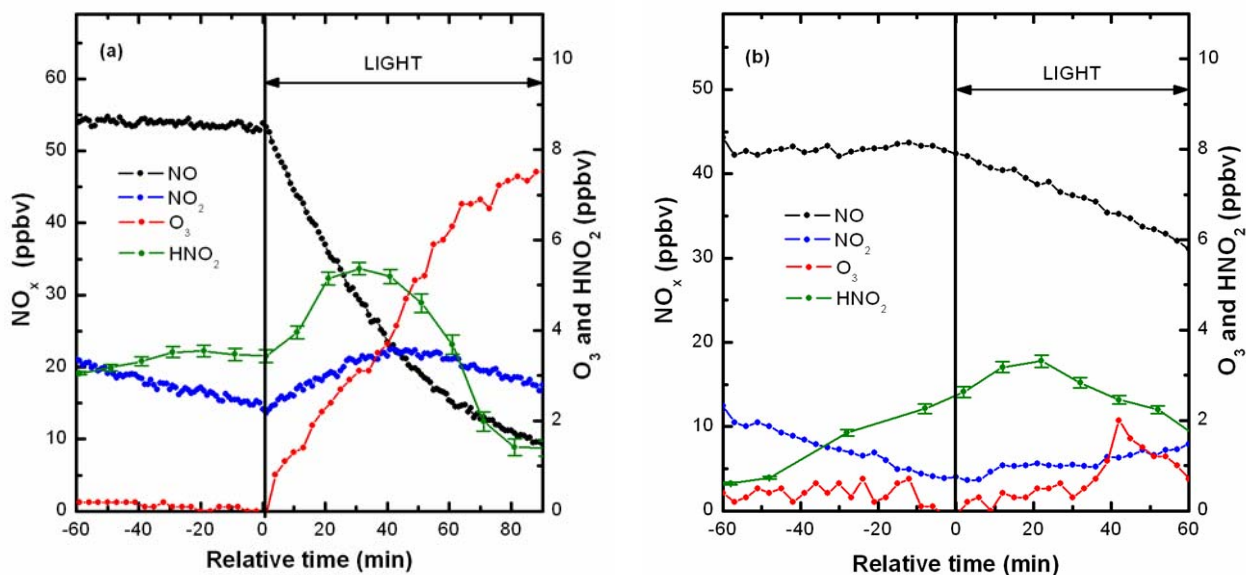
Hence, for low mixing heights i.e. 50 m (or in other words for close vicinity of buildings), the removal by active depolluting material can compete with the other homogeneous removal pathways if 10% or more of the building are covered with TiO<sub>2</sub>. Moreover, if 40% of urban surfaces or more is activated then the heterogeneous removal may dominate over OH reaction and photolysis. Therefore this hypothetical exercise showed that implementing TiO<sub>2</sub> based construction materials, can for the specific case of HCHO be a significant sink term potentially improving urban air quality.



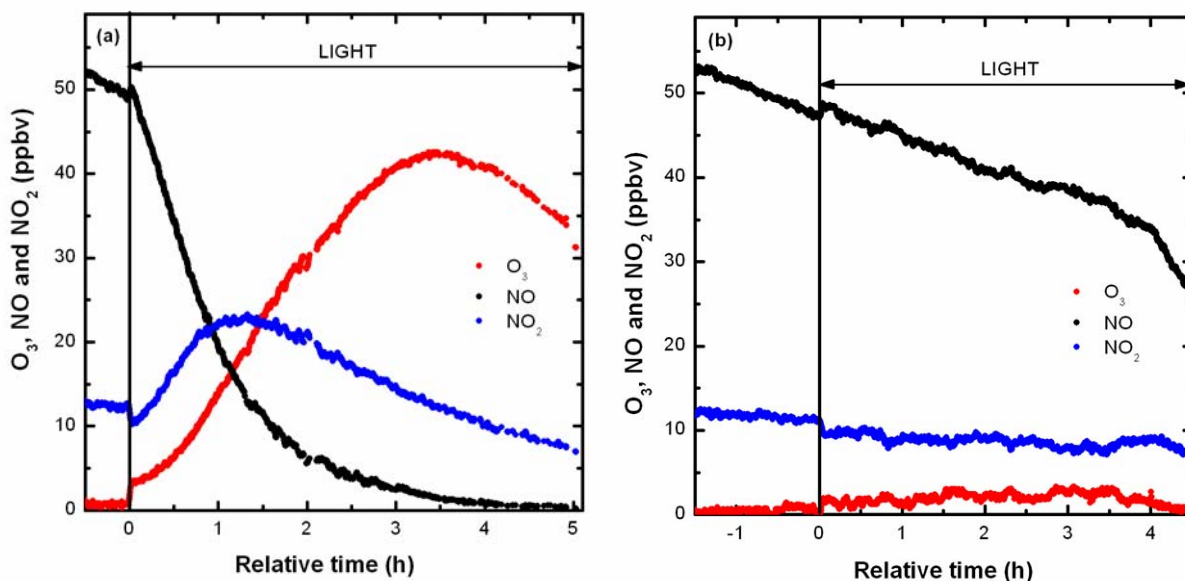
**Figure 17:** Lifetimes of HCHO due to photolysis, reaction with OH<sup>-</sup> and deposition process onto mineral surfaces. The latter trends are represented as a function of surface covered by TiO<sub>2</sub> coatings for different air mixing heights (ranging from 50 m to 500 m).

### III.3 Ozone formation on titanium dioxide coated glasses

After introduction of synthetic air and NO into the CESAM chamber, the concentrations of NO, NO<sub>2</sub>, HNO<sub>2</sub> and O<sub>3</sub> are monitored in the dark for one hour. Then the artificial illumination is turned on and the chemical system is again monitored for 90 minutes. A similar procedure is adopted for the Teflon outdoor chamber using natural illumination. After flushing dry purified air, known amounts of NO and NO<sub>2</sub> are injected and the NO, NO<sub>2</sub> and O<sub>3</sub> concentrations are monitored for 30 minutes in the dark. The reactor is then exposed to natural light and the gas mixture evolution is followed for 4 hours. The results for a TiO<sub>2</sub> coated glass and for a standard glass studied with the CESAM and the outdoor chamber are displayed in Figures 18 and 19, respectively.

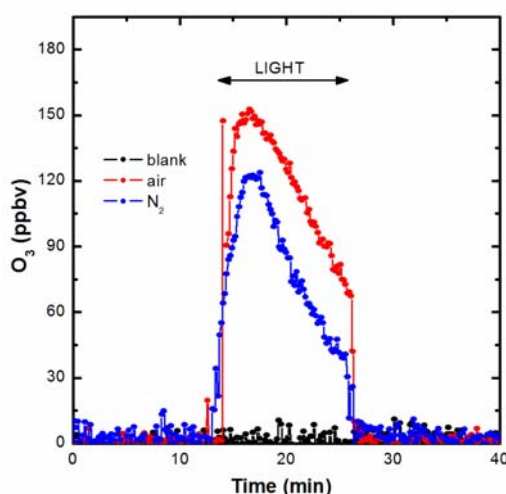


**Figure 18.** NO, NO<sub>2</sub>, HNO<sub>2</sub> and O<sub>3</sub> profiles recorded in the presence of (a) a TiO<sub>2</sub> coated glass and (b) a standard glass in the CESAM chamber. The vertical line indicates the moment when the light was turned on.



**Figure 19.** NO, NO<sub>2</sub> and O<sub>3</sub> profiles under natural irradiation in the presence of (a) a TiO<sub>2</sub> coated glass and (b) a standard glass in the outdoor chamber. The vertical line indicates the moment when the chamber was exposed to natural illumination.

Despite the different time scales, illumination type and chambers building material, the observed trace gases evolution is similar. In agreement with previous studies,<sup>93</sup> NO uptake on the TiO<sub>2</sub> coated glass is enhanced under irradiation decreasing with time in both experiments. The NO<sub>2</sub> concentration profile exhibits a maximum under illumination, suggesting that it is formed from NO photocatalytic oxidation and then converted into HNO<sub>3</sub> and HNO<sub>2</sub> at the surface.<sup>24,37-39,43</sup> At the same time a significant accumulation of ozone is observed. In agreement with previous studies,<sup>24,37,38,94</sup> HNO<sub>2</sub> production is enhanced under irradiation in presence of TiO<sub>2</sub> (Figure 19). However, when a standard glass is analyzed in both chambers, no ozone formation is detected (Figures 18b and 19b). As well the NO<sub>2</sub> and NO concentration profiles are similar for the standard glass and the empty outdoor chamber with no evidence of a light effect (Figures 19b). These results indicate that O<sub>3</sub> formation can not be explained by the gas phase chemistry occurring in the chambers. The differences between the O<sub>3</sub> profiles obtained for the blank experiments and the coated glass suggested that TiO<sub>2</sub> should be involved in the reaction mechanism leading to O<sub>3</sub> formation via heterogeneous reaction. But simulation chamber experiments are not concluding about the processes that lead to the results obtained.



**Figure 20.** Effect of light (8 near-UV emitting lamps in the 300-420 nm wavelength range) on a TiO<sub>2</sub> / KNO<sub>3</sub> (50 % w/w) film using synthetic air and pure N<sub>2</sub> as carriers. The same blank signal was given by an empty tube and by a tube with a KNO<sub>3</sub> deposit using both carriers.

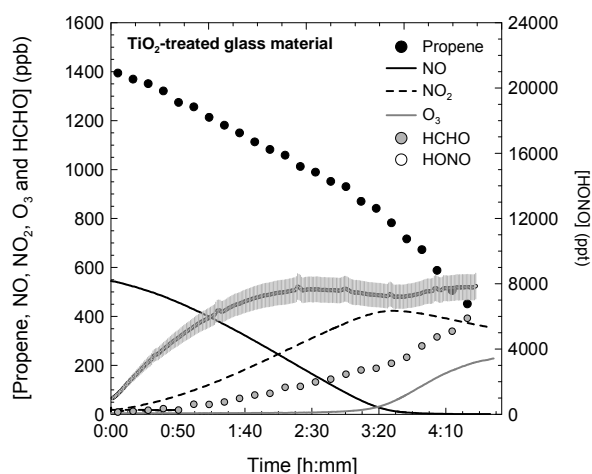
To investigate the origin of the observed O<sub>3</sub> increase a second type of experiment has been carried out using a flow tube reactor. It is well known that nitrate anions are formed as a consequence of the photocatalytic oxidation of NO<sub>2</sub> on UV-illuminated TiO<sub>2</sub> surfaces,<sup>14,23,40-43</sup>. Therefore, film of TiO<sub>2</sub> / KNO<sub>3</sub> 50 % w/w has been exposed to near-UV irradiation using synthetic air or pure N<sub>2</sub> as carrier gases (Figure 20). As described previously, a renoxification process occurs on illuminated TiO<sub>2</sub> films mixed with nitrate<sup>44,94</sup>. In contrast with the mechanism proposed by Grassian and co-workers<sup>45,95</sup> for a film composed by nitrate and aluminium oxide, under the experimental condition used (weak UV radiation) nitrate photolysis is negligible (Figure 20). An alternative renoxification pathway (1-3) including the photochemistry of the NO<sub>3</sub> radical can explain the release of NO and NO<sub>2</sub> from the illuminated TiO<sub>2</sub> surfaces,<sup>44</sup> and the further formation of O<sub>3</sub>. The following mechanism can also explain the relative higher concentration of O<sub>3</sub> produced with O<sub>2</sub> as carrier gas:

$\text{NO}_3^- + h\nu_{\text{vb}} \rightarrow \text{NO}_3^\bullet$	(17)
$\text{NO}_3^\bullet + \text{NO} \rightarrow \text{NO}_2 + \text{NO}_2^\bullet$	(18)
$\text{NO}_3^\bullet + \text{NO}_2 \rightarrow \text{NO}_2 + \text{O}^\bullet$	(19)
$\text{O}^\bullet + \text{O}_2 \rightarrow \text{O}_3$	(20)
$\text{NO}_3^\bullet + \text{O}_2 \rightarrow \text{NO}_2 + \text{O}_3^\bullet$	(21)

Although O<sub>3</sub> has been recently proved to decompose on illuminated TiO<sub>2</sub> surfaces;<sup>96</sup> its formation is observed when TiO<sub>2</sub> treated surfaces are exposed to NO<sub>x</sub> under illumination. This difference can be explained by a renoxification process involving the photochemistry of the NO<sub>3</sub> radical. Even if majority of the studies<sup>14,23,40-43</sup> argue that nitrate is an innocuous final product of the photocatalytic NO<sub>x</sub> removal process, the present work demonstrates for the first time that O<sub>3</sub> can actually be formed on TiO<sub>2</sub> glasses coated by nitrate. The heterogeneous reactions carried out on the surface of TiO<sub>2</sub> containing materials indicate that new remediation technologies based on these materials may not have the desired impact on the environment and human health.

### III.4 the influence of TiO<sub>2</sub> coating on the chemistry of propene/NO<sub>x</sub>/light system under atmospheric conditions

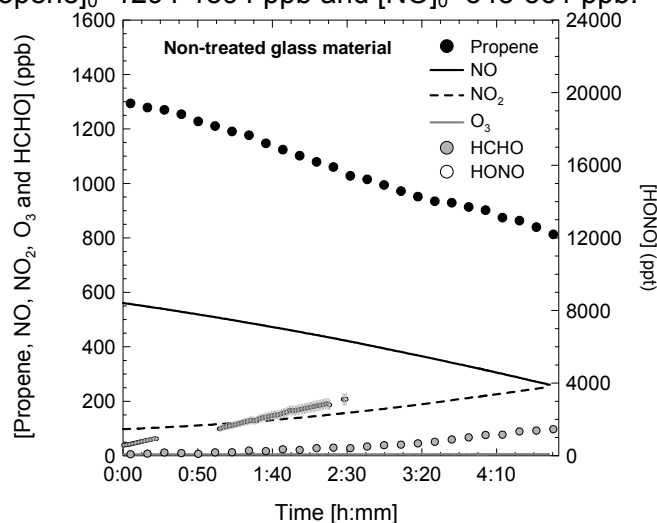
Two series of experiments have been conducted: At ICARE relatively high concentration were used (i.e around 1.3 ppm of propene and 700 ppb of NO<sub>x</sub>) while at LISA the initial concentrations were ranging from 150 to 400 ppb in VOC and from 50 to 100 ppb in NO<sub>x</sub>. In total 15 experiments were carried out.



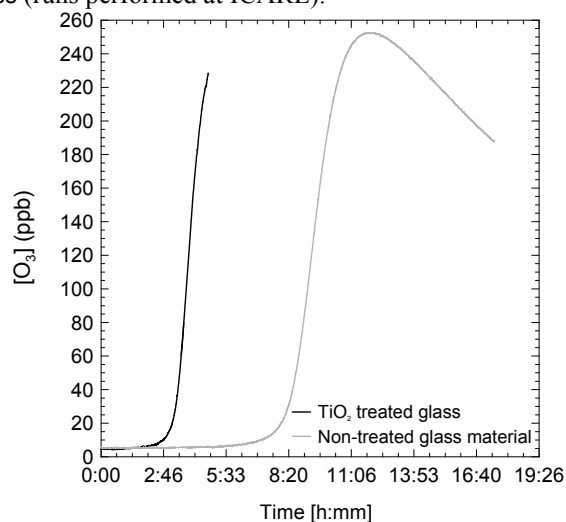
**Figure 21** : Concentration-time profiles of reactants and oxidation products in the propene/NO/air/light system in the presence of TiO<sub>2</sub> treated glass. (runs performed at ICARE).



Test runs were first conducted to check the behaviour of NO and/or propene in absence of glass plates with and without irradiation. The decrease of the concentrations of these species versus time was found to be similar to that due to dilution. Figures 21 and 22 show examples of the experimental concentration-time profiles of the reactants (NO and propene) and the observed products, respectively, with the non-TiO<sub>2</sub>-treated and with the TiO<sub>2</sub>-treated glass plates when initial concentrations were [propene]<sub>0</sub>=1294-1394 ppb and [NO]<sub>0</sub>=545-561 ppb.

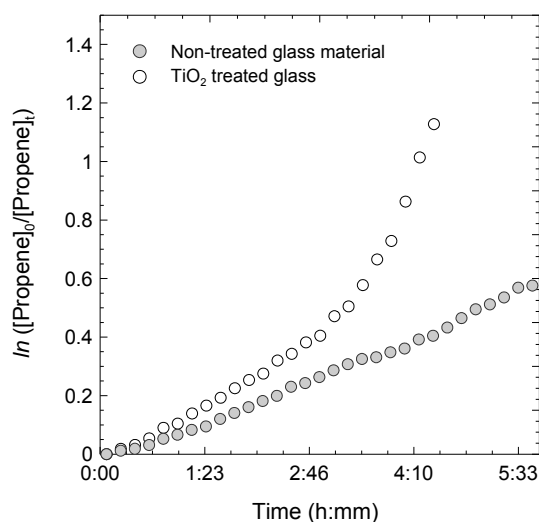


**Figure 22 :** Concentration-time profiles of reactants and oxidation products in the propene/NO/air/light system in the presence of non-TiO<sub>2</sub>-treated glass (runs performed at ICARE).

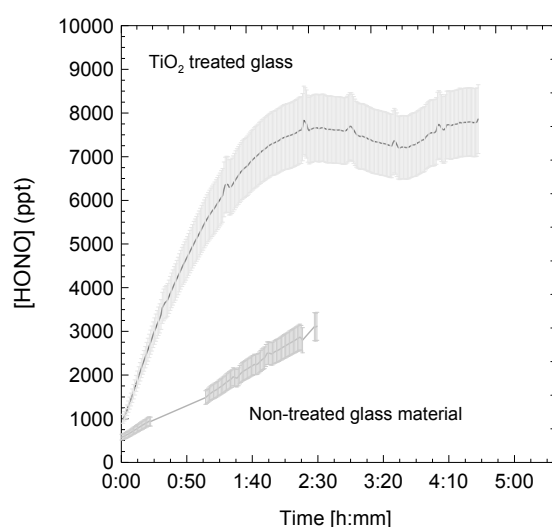


**Figure 23 :** Concentration-time profiles of O<sub>3</sub> under different conditions during photo-oxidation propene/NO experiment (runs performed at ICARE).

These results indicate that there is a significant additional loss of propene and NO in the presence of TiO<sub>2</sub>-treated glass materials in comparison with their loss in the presence of non treated glass materials. In the first two and a half hour of the run (i.e before any significant production of ozone) only 250 ppb of propene is consumed for the non-treated glass while around 400 ppb have been consumed for the TiO<sub>2</sub>-containing material. For NO concentration-photolysis time profiles, photocatalytic effect is even more pronounced where 99% has disappeared for the treated-glass material and only 43% for the non-treated glass materials in the first four hours. In a second part of the experiment, one can notice a significant ozone production which lead to an additional loss of propene due to ozonolysis in the case of TiO<sub>2</sub>-treated material. In the case of non-treated glass, the ozone formation is significantly delayed as shown in Figure 23 due to the fact that a much longer reaction time is necessary in such a system to reach a low NO level. Nevertheless, as soon as ozone accumulation starts, it shows very similar efficiencies in both systems.



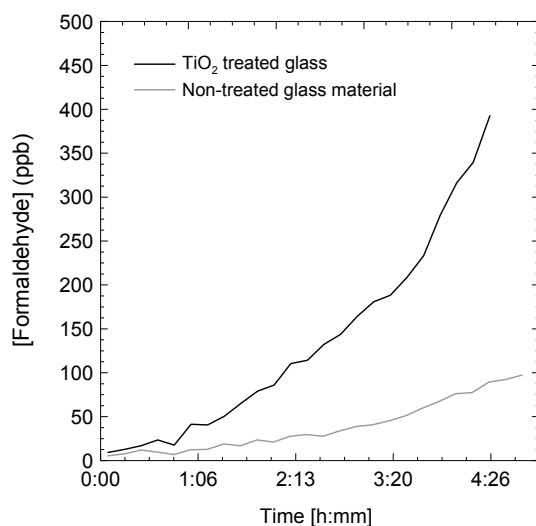
**Figure 24 :** The loss of propene under different conditions during photo-oxidation propene/NO experiment.



**Figure 25 :** Concentration-time profiles of HONO under different conditions during photo-oxidation propene/NO experiment.

Test experiments have been carried out with propene alone irradiated in the presence of  $\text{TiO}_2$  treated glass. They have shown that no significant additional propene losses could be observed. This supports the fact that, in such chemical system, the two main propene loss processes are reaction with OH and with ozone. [Figure 25](#) shows a rough analysis of the propene loss during the experiments. Assuming a pseudo first order behaviour (i.e. constant radical concentration),  $\ln([\text{propene}]_0/[\text{propene}])$  was plotted as a function of the irradiation time. The figure shows a linear increase in the consumption of the propene as the reaction goes with a larger slope in the presence of the treated surfaces compared to the non-treated ones. The time-concentration profile deviates from the linearity for longer reaction time in the case of the treated surfaces. This can be attributed to the increase of ozone concentration as the reaction goes. The slope of the first part of the curve when  $\text{TiO}_2$  treated glass was used is 50% larger than with normal glass which indicates that OH levels were 50% higher in the case of photocatalytically active glass. This observation might be correlated with the fact that nitrous acid (HONO) was also formed ([Figure 25](#)), reaching a concentration which was 2.5 times higher for the  $\text{TiO}_2$ -material than for the non-treated glass material, leading to a final concentration around 8 ppb in the presence of treated material.

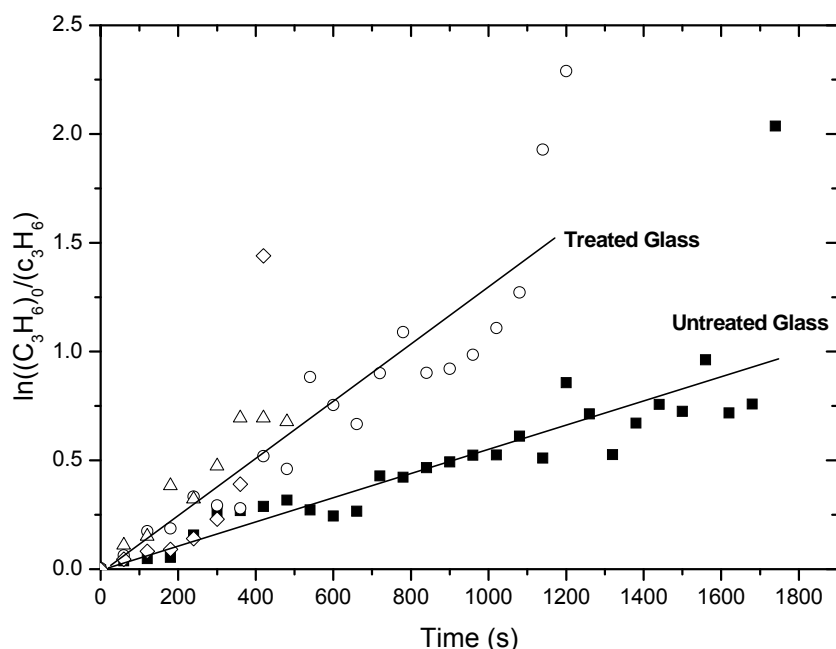
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**Figure 26** : Concentration-time profiles of Formaldehyde under different conditions during photo-oxidation Propene/NO experiment.

Formaldehyde was also observed as oxidation product where 72 ppb was formed in the presence of non-treated material while higher concentration was obtained for the treated material, reaching 309 ppb for 4 hours reaction time scale (Figure 26).

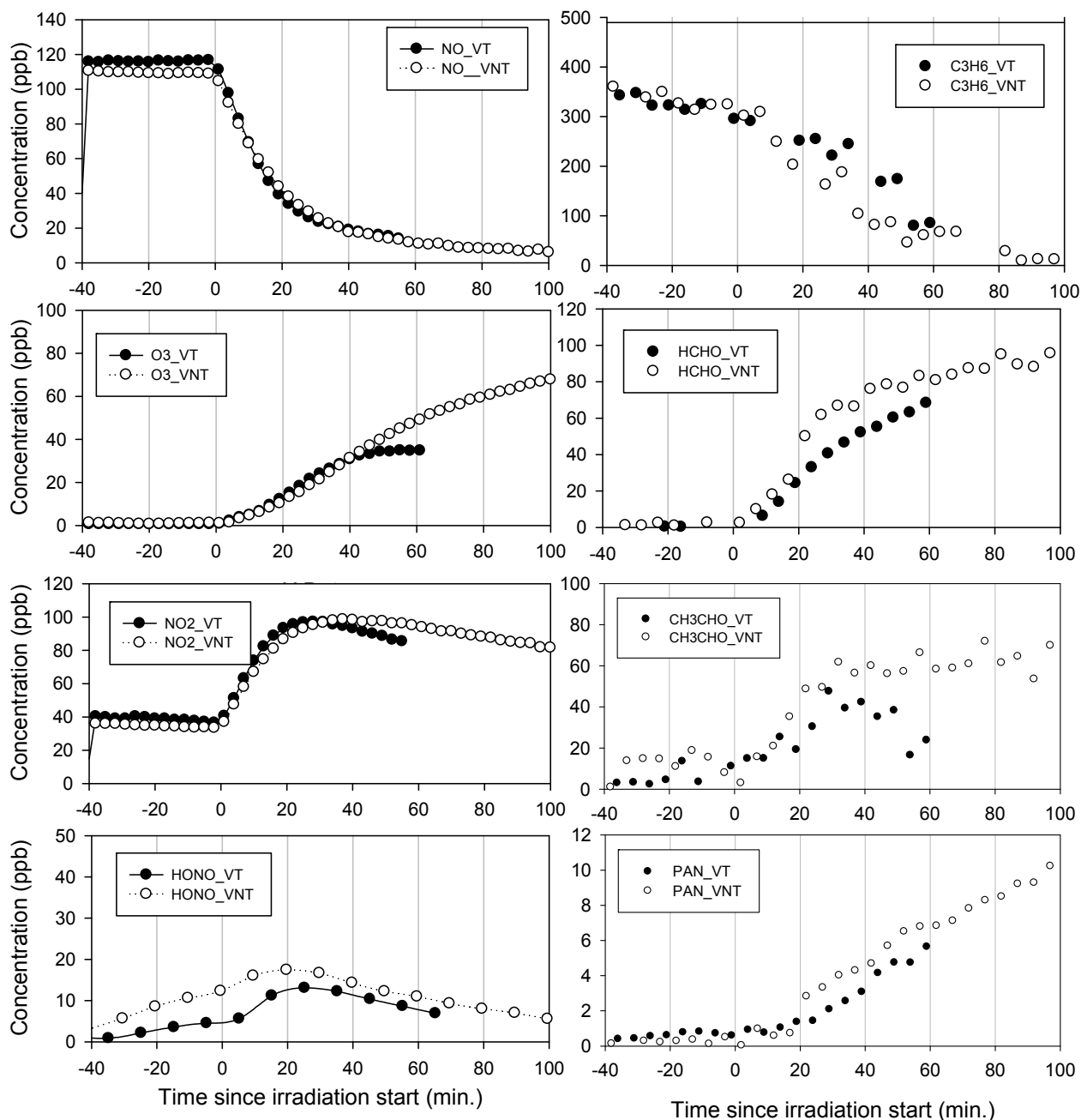
Several experiments were carried out at lower concentration. At this much atmospherically relevant levels, the effect were found less obvious. Nevertheless, similar conclusion than those arising from ICARE experiment can be drawn. As shown on figure 27, when 50 ppb of NO was initially used the pseudo-first order of the propene loss was two time larger in the presence of TiO<sub>2</sub> coated glass that with normal glass.



**Figure 27** : Pseudo-first order plot of the propene loss in the presence of non-treated and treated material

The comparison of concentration-time profiles recorded for both materials given in figure 28 shows that under these conditions the two conditions lead to very similar observations. This can be easily explained by the fact that the effect of TiO<sub>2</sub> material on nitrogen oxides is a function of NO<sub>x</sub> levels itself. It is hence not surprising that at lower NO<sub>x</sub> conditions the effect was smaller. Nevertheless, a very interesting additional effect was recorded during these experiments. Indeed, even if the ozone production rate is very similar during the first 40 minutes of the experiment, a

unexpected plateau is reached with treated glass while the ozone production remains in the case of non-treated materials. The reason for this behaviour is not clear and further investigations are needed. Nevertheless one can make the hypothesis that secondary products involved in ozone production when propene concentration becomes low are trapped by photocatalytic surfaces and no more available in the gas phase.



**Figure 28 :** Concentration-time profiles of reactants and products during a low concentration simulation experiment performed at LISA in the presence of treated glass (black symbols) or non-treated glass (empty symbols). Time origin is taken when light was turned on.

## IV. CONCLUSIONS

The reactivity of NO<sub>2</sub> on irradiated TiO<sub>2</sub> / SiO<sub>2</sub> films was studied, with different TiO<sub>2</sub> contents, as proxies for NO<sub>x</sub> de-polluting materials. The influence of the photocatalyst concentration, the role of molecular oxygen and the effect of nitrate on the reactivity of TiO<sub>2</sub> films were investigated. NO, HONO and nitrate anions are produced as a consequence of the NO<sub>2</sub> loss on UV-illuminated TiO<sub>2</sub> films. A renoxification pathway that involves the photochemistry of the NO<sub>3</sub> radical leads to the release of NO, NO<sub>2</sub> and of HONO from the TiO<sub>2</sub> surface. The presence of O<sub>2</sub> in the carrier gas modifies the NO and HONO production yields in the heterogeneous reaction between NO<sub>2</sub> and TiO<sub>2</sub> as well as the products of the renoxification process.

The kinetics of the heterogeneous reaction between gaseous HCHO and TiO<sub>2</sub>/SiO<sub>2</sub> mineral coatings have been investigated to mimic HCHO loss on TiO<sub>2</sub> coated depolluting urban surfaces, by means of flow tube studies. The measured uptake kinetics were observed to be strongly enhanced when the surface (or coating) was irradiated in the wavelength range from 340 to 420 nm (with an irradiance of 1.45 mW cm<sup>-2</sup>). The associated BET uptake coefficients were measured in the range from  $(3.00 \pm 0.45) \times 10^{-9}$  to  $(2.26 \pm 0.34) \times 10^{-6}$  and were strongly dependent on the HCHO initial concentration in the range from 3.5 to 32.5 ppbv, relative humidity from 6 to 70%, temperature from 278 to 303 K and TiO<sub>2</sub> content in the mineral coating from 1 to 100% wt. The measured kinetics were well described using a Langmuir-Hinshelwood type formalism. The estimated uptake coefficients were used to discuss the importance of the heterogeneous HCHO surface loss, in terms of deposition lifetimes, as compared to major homogeneous gas phase losses (OH reaction and photolysis). It is found that deposition may compete with gas phase removal of HCHO in a dense urban environment if more than 10% of urban surface is covered with TiO<sub>2</sub> treated materials.

Experiments were conducted at high and low concentrations on the photooxidation of gas mixture propene/NO chosen as a model for VOCs atmospheric oxidation. These results show that the photocatalytic effect of TiO<sub>2</sub> can affect the oxidative capacity of the gas phase composition. They also show that these effects are non linear and ambiguous as they affect strongly the NO/NO<sub>2</sub>/HONO system which is the heart of the ozone production scheme. In order to assess an affect at larger scale on photo-oxidant concentration, additional experiments coupled with computer simulations are needed.

Indeed, this project has produced the basic physico-chemical parameters required to build consistent mechanism taking into account the complex interaction of photo-catalytical surfaces with their atmospheric environment. It is now possible and necessary to draw models which will help to quantify the effect of the competition or the synergy between these new processes and the fluid dynamic at street or urban scale.

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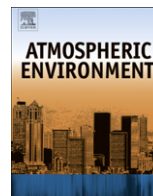
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## Kinetics of the tropospheric formaldehyde loss onto mineral dust and urban surfaces

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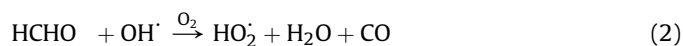
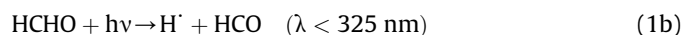
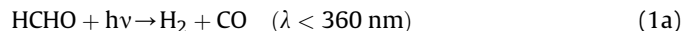
## ABSTRACT

The kinetics of the heterogeneous reaction between gaseous HCHO and TiO<sub>2</sub>/SiO<sub>2</sub> mineral coatings were investigated using a coated-wall flow tube to mimic HCHO loss on mineral aerosol and TiO<sub>2</sub> coated depolluting urban surfaces. The measured uptake kinetics were strongly enhanced when the flow tube was irradiated with 340–420 nm UV light with an irradiance of 1.45 mW cm<sup>-2</sup>. The associated BET uptake coefficients ranged from  $(3.00 \pm 0.45) \times 10^{-9}$  to  $(2.26 \pm 0.34) \times 10^{-6}$  and were strongly dependent on HCHO initial concentration, relative humidity, temperature, and TiO<sub>2</sub> content in the mineral coating, which ranged from 3.5 to 32.5 ppbv, 6–70%, 278–303 K, and 1–100 %wt, respectively. The measured kinetics were well described using a Langmuir–Hinshelwood type formalism. The estimated uptake coefficients were used to discuss the importance of heterogeneous HCHO surface loss, in terms of deposition lifetimes, as compared to major homogeneous gas-phase losses such as OH reaction and photolysis. It is found that deposition may compete with gas-phase removal of HCHO in a dense urban environment if more than 10% of the urban surface is covered with TiO<sub>2</sub> treated material.

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## 1. Introduction

Formaldehyde (HCHO) is an important and highly reactive compound present in all regions of the atmosphere, arising from the oxidation of biogenic and anthropogenic hydrocarbons, and is a key compound in tropospheric chemistry. It is a strong HO<sub>x</sub> source (through its photolysis) and is therefore strongly connected to regional O<sub>3</sub> production. The main HCHO removal processes from the atmosphere are currently thought to be its photolysis and the reaction with OH according to (Atkinson, 2000):



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These removal processes are homogeneous and will happen throughout the troposphere. However, it is also known that HCHO is chemically taken up in the atmosphere by sulphuric acid aerosols (Iraci and Tolbert, 1997). Therefore, it is worth investigating whether similar heterogeneous reactions may occur on other surfaces such as mineral surfaces or buildings.

At the global scale, mineral dust aerosol relates to climate, biogeochemical cycles (Andy, 2002), human health (Derbyshire, 2007) as well as atmospheric chemistry (Dentener et al., 1996). In fact, dust surfaces exposed to trace gases may promote chemical reactions that do not occur in purely homogeneous media. Recently, we showed that the uptake of otherwise unreactive gases (i.e., O<sub>3</sub> and NO<sub>2</sub>) is strongly enhanced on mineral oxide surfaces (Ndour et al., 2008a,b) and may be related to traces of TiO<sub>2</sub> present in dust particles irradiated with UV light. A similar enhancement could exist for HCHO conversion on mineral dust surfaces.

At the local scale, air pollution and NO<sub>x</sub> levels due to traffic is one of the most pressing problems in urban areas. In order to adhere to regulations requiring a reduction in emissions, the use of photocatalytic self-cleaning and “depolluting” materials has been suggested in recent years as a remediation technique in polluted urban environments (Fujishima and Hashimoto, 1996). Some of these commercial products are based on the photocatalytic

properties of TiO<sub>2</sub>, which when exposed to sunlight may help in the abatement of atmospheric NO<sub>x</sub>. The use of TiO<sub>2</sub> photocatalysis as an environmentally friendly pollution control technology has been reported in many European areas; specifically, a thin layer of TiO<sub>2</sub> can be either deposited at the surface of a material (such as glass or pavement) or embedded in paints constituents and concrete (Beeldens and Van Gemert, 2005; Fujishima and Hashimoto, 1996; Stephan and Wilhelm, 2006), and its applications include not only depollution but also surface maintenance (Van and Montgomery, 1998; Basel, 2008).

Despite the importance of HCHO interactions with TiO<sub>2</sub> surfaces under atmospheric conditions, the details of these reactions are not yet documented. Several previous studies have described the reaction in the dark between HCHO and metals (such as aluminium) (Kieu et al., 2001; Saleh and Hussain, 1986) or some inorganic oxides (such as aluminium oxide Al<sub>2</sub>O<sub>3</sub> and ferric oxide Fe<sub>2</sub>O<sub>3</sub>) (Lur'e and Mikhno, 1999; Xu et al., 2006), as proceeding quite slowly due to weak adsorption of HCHO on such surfaces at ambient temperature. Similar experiments have demonstrated that HCHO reacts with some mineral oxides at 295 K with high initial uptake coefficients that rapidly decreases on the time scale of a few minutes (Carlos-Cuellar et al., 2003; Grassian, 2001; Li et al., 2001; Usher et al., 2003). Other studies (Liu et al., 2005; Obee and Brown, 1995) focused on the photocatalytic degradation of HCHO on pure TiO<sub>2</sub> coatings or TiO<sub>2</sub>-Fe<sub>2</sub>O<sub>3</sub> mixtures (Yang et al., 2000) at high HCHO concentrations (0.5–100 ppmv), which are not representative of atmospheric conditions or dust composition. Hence, to our knowledge, little is known about the heterogeneous chemistry of HCHO on mineral oxide surfaces or its overall significance in the atmosphere.

Accordingly, the objective of this work was to investigate whether surface reactions on mineral coatings containing variable amount of TiO<sub>2</sub> could be a significant tropospheric sink of HCHO in both the free troposphere (mineral dust containing traces up to 5 %wt of TiO<sub>2</sub>) and urban environments (almost pure TiO<sub>2</sub>). In this study, we used a coated-wall flow tube to investigate the uptake kinetics of HCHO onto coatings composed of TiO<sub>2</sub>/SiO<sub>2</sub> mixtures. We also examined the effect of temperature, relative humidity, HCHO concentration and TiO<sub>2</sub> content on the uptake coefficient. The measured uptake coefficients at pure TiO<sub>2</sub> surfaces were used to assess the case of HCHO loss in an urban environment through dry deposition processes. In this manner, HCHO deposition lifetimes were calculated and compared to major photochemical HCHO removal pathways.

## 2. Experimental section

### 2.1. Mineral oxides: preparation and characterization

Experiments were performed with different mass mixing ratios of mineral oxides, in the range from 1 to 100 %wt, by diluting titanium dioxide TiO<sub>2</sub> (Degussa-P25, 80% anatase, 20% rutile; P25) in silica SiO<sub>2</sub> (Degussa Aerosil 130). All mixtures were prepared by suspending 3 g of the mineral oxides in 30 mL of ultra pure water (Aquadem milli-Q50). A few milliliters of the sonicated suspensions were dripped uniformly into dry Pyrex tubes (20 cm × 1.1 cm i.d.) that were then rotated and dried at 373 K. The resulting film covered the entire inner surface of the tube and, to the eye, was fairly uniform in thickness.

Characterization of the dried film was performed using scanning electron microscopy (SEM) coupled to energy dispersive X-ray spectroscopy (EDX). For this purpose, the Pyrex tubes were cut into 1-cm long samples (considering finally only both ends and middle parts of the tube) and dipped vertically into a mould containing an epoxy resin (araldite epoxy CY 230-ESCIL) and an epoxy resin

hardener (HY 956-ESCIL) in a ratio of 2.5:1 (resin:hardener). After 12 h, the mixture dried and hardened, forming a polymer at room temperature. The polymer section (holding the tubes) was then polished (ESC 200 GTL polisher from ESCIL) for better image resolution. Finally, these SEM samples were coated with a thin layer of gold to enable electron conduction to the observed area. Films with different TiO<sub>2</sub> mixing ratios (1, 5, 50 and 100 %wt) were observed. In addition, the analysis of different zones confirmed the uniformity of the film along the length of the tube for each sample. Film thicknesses ranged from 20 to 30 μm. Fig. 1 shows both the SEM image of a TiO<sub>2</sub>/SiO<sub>2</sub> coating (50 %wt) (part a) and the surface profile of an area scanned from 0 (the Pyrex surface) to 40 μm (polymer matrix) (part b). It is clear that the film adheres strongly to the Pyrex surface, fitting with any surface defect (see Fig. 1a). The EDX detection of the yellow line scanned in Fig. 1a corroborates the film's chemical composition. More specifically, there are two successive silicon signal in the scanning profile from the Pyrex surface to the polymer matrix, which are due to the Pyrex composition (higher peak) and to the coating (lower peak). The titanium signal begins at a distance of 11 μm and extends to 35 μm (Fig. 1), thus indicating a film thickness of 24 μm. It reaches the concentration of the lower silicon peak since both TiO<sub>2</sub> and SiO<sub>2</sub> are equally distributed in the film (TiO<sub>2</sub> 50 %wt/SiO<sub>2</sub> 50 %wt coating). Note that the Ti and Si concentrations are estimated to 15 %wt of the coating as the gold deposited at the SEM sample is also detected. The cartography of another 50 %wt TiO<sub>2</sub> sample scanned from the Pyrex glass tube (right) to the film (left) (shown with a 4000 magnification in Fig. 1c) proves that the Ti and Si atoms are equally and homogeneously distributed in a 50 % TiO<sub>2</sub> film.

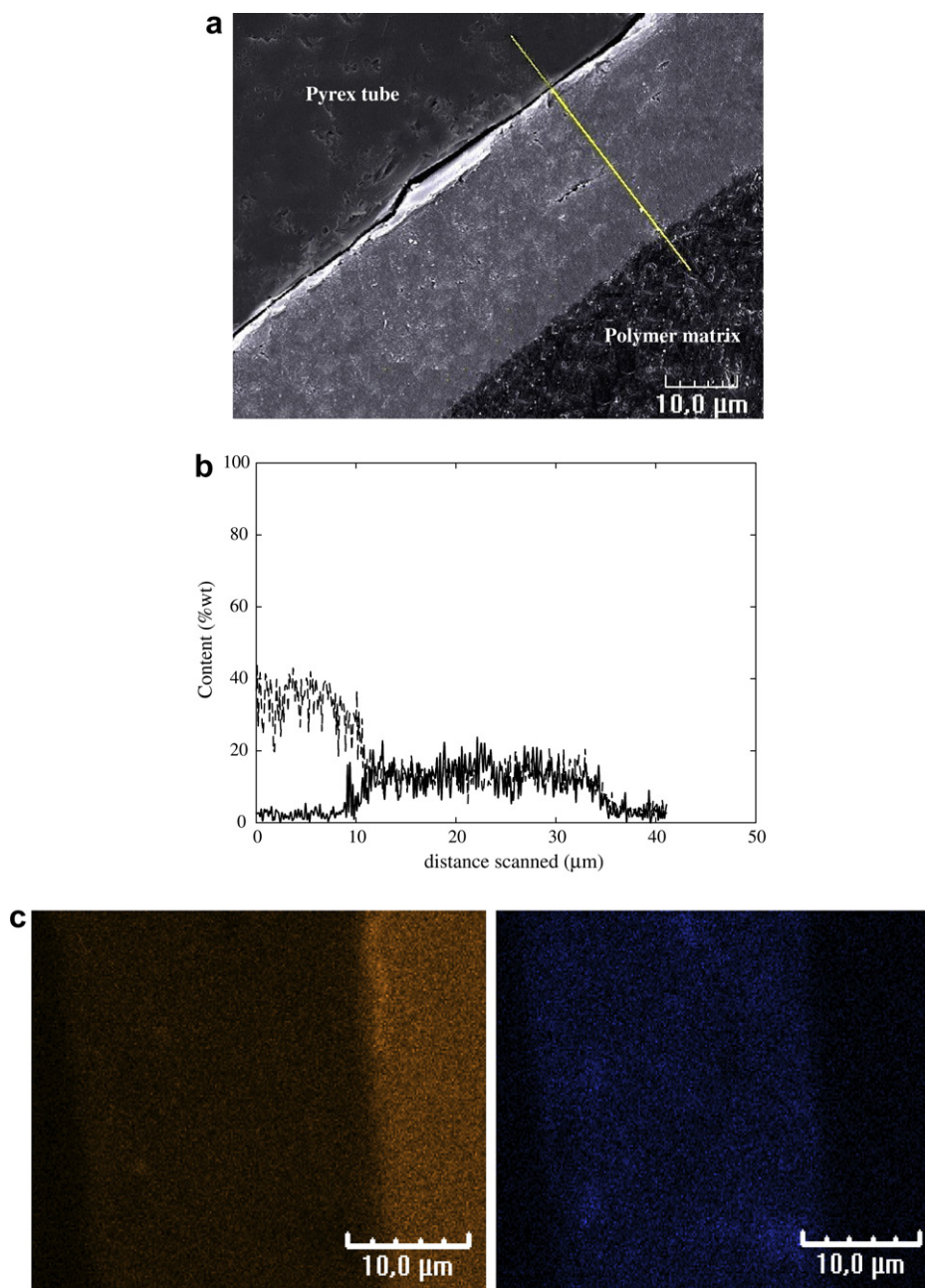
### 2.2. Flow tube reactor

The heterogeneous interactions between formaldehyde and mineral surfaces were studied by exposing films of TiO<sub>2</sub>/SiO<sub>2</sub> mixtures to known HCHO concentrations. All experiments were performed under atmospheric pressure and at constant temperature in a reactor described elsewhere (Jammoul et al., 2008). A cylindrical Pyrex tube coated with the reactive surface and not used for imaging was introduced into the constant-temperature reactor, which was surrounded with fluorescent lamps (UV Black-Light-Blue OSRAM Sylvania TLD 15W/08) emitting in the spectral range between 340 and 420 nm with λ<sub>MAX</sub> = 365 nm. The spectral irradiance E(λ) reaching the inner surface of the reactor has been quantified previously (Jammoul et al., 2008). The gas flows (N<sub>2</sub>) were controlled by mass flow controllers (Brooks electronic). All gases were introduced into the reactor via a tubular movable injector (0.3 cm outer radius ending with a porous section). Using a total gas flow of 500 mL min<sup>-1</sup>, no gas-phase photodissociation of HCHO was observed, and laminar flow conditions were established within the first centimetre of the flow tube (Re < 100).

### 2.3. HCHO generator and analyzer

Gaseous formaldehyde was introduced into the reactor in a flow of nitrogen through a home-made silicon permeation tube immersed in a 3.7 %wt HCHO solution. The temperature was held at 298 K, and the relative humidity exiting the permeation tube was ca. 6%.

The gas flow exiting the reactor was monitored with a portable HCHO analyzer developed at IRCELYON (Sassine et al., in preparation). In this novel analyzer, formaldehyde is stripped out of the gas flow via a glass tube sampler and undergoes derivatization with 3-Methyl-2-benzothiazolinone hydrazone (MBTH) in two successive steps in order to form a strongly absorbing chromophore



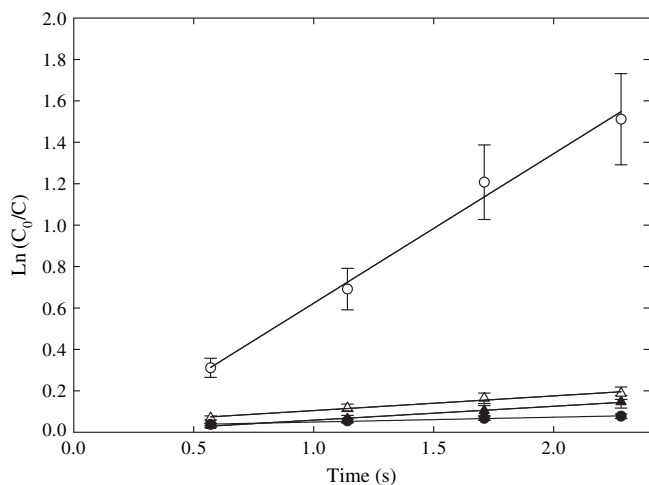
**Fig. 1.** (a) SEM image showing the interface of 50 %wt TiO<sub>2</sub>/SiO<sub>2</sub> coating, (b) Surface profile of the yellow line scanned in part (a) displaying Ti (full line) and Si (dashed-line) concentrations (c) Cartography of another 50 %wt TiO<sub>2</sub> coating showing Ti (blue) and Si (yellow) distribution in the film.

(Sawicki et al., 1961). The detection, in solution, of the converted HCHO was realized by means of a combination of a spectrograph (Andor technology/Shamrock SR – 163 i) coupled to a CCD camera (Andor Technology/iDus DV-420). Teflon AF2400 tubing (Biogeneral) was used as the UV–vis long path cell (Dasgupta et al., 1998). Combining the strongly absorbing chromophore with a 100-cm long optical path led to a detection limit of ca. 3 pptv with a resolution time of 15–30 min. These formaldehyde measurements were validated against optical and chromatographic methods. Calibrations with Differential Optical Absorption Spectroscopy (DOAS) and Fourier transform infrared spectroscopy (FTIR) showed less than 6% deviation. Similar results were found when HCHO measurements were compared with those obtained using liquid chromatography coupled to UV-DAD detection subsequent to

DNPH titration, and were independent of the method between Sepack cartridges (Grosjean, 1991) and Radiello passive tubes trapping techniques (Clarisse et al., 2003).

#### 2.4. Kinetic analysis

The uptake rate of HCHO on the mineral surfaces was determined by monitoring its loss in the gas phase as a function of the position of the movable injector, i.e., as a function of the exposure time of the oxide surface to the gas. The linear fit (Fig. 2) of the measured HCHO concentrations at different exposure times is typically used to derive an apparent pseudo-first-order coefficient ( $k_{\text{obs}}$ ) for HCHO decay.



**Fig. 2.** Kinetic of logarithmic HCHO decay as a function of residence time for 11 ppb of HCHO, at 298 K at 6% of RH on different films mixing ratios. Circles and triangles correspond to measurements performed with pure TiO<sub>2</sub> and pure SiO<sub>2</sub> coatings respectively. Open and dark symbols are assigned to illuminated and dark conditions.

$$k_{\text{obs}} = \frac{1}{4} \gamma_{\text{BET}} \times \langle c \rangle \times \left( \frac{S_{\text{BET}}}{V_{\text{tube}}} \right) \quad (3)$$

Consequently, HCHO lifetime can be approximated as follows:

$$\tau = \frac{1}{k_{\text{obs}}} = \left( \frac{V_{\text{tube}}}{S_{\text{BET}}} \right) \times \frac{4}{\gamma_{\text{BET}} \times \langle c \rangle} \quad (4)$$

where  $k_{\text{obs}}$  is the observed rate constant of the reaction,  $\langle c \rangle$  is the mean molecular speed of gaseous HCHO, and  $V_{\text{tube}}$  is the volume of the flow tube.  $S_{\text{BET}}$  is the BET area of the entire inorganic sample exposed to gas interaction and  $\gamma_{\text{BET}}$  is the mass-independent uptake coefficient taking into account the entire sample surface (not just the geometric upper-most surface) (Grassian, 2001; Michel et al., 2003; Underwood et al., 2000, 2001). A linear dependence of the observed uptake rate on sample mass was observed, indicating that the use of BET sample area is appropriate in the calculation of the uptake coefficient.

The experimental data presented in the paper have been corrected for diffusion limitation using the Cooney–Kim–Davis (CKD) method, (Behnke et al., 1997; Cooney et al., 1974), which takes into account axial and lateral diffusion combined with a first-order loss at the inner surface of a cylindrical tube under laminar flow conditions. The diffusion coefficient was calculated using the formula proposed by Fuller et al. (Fuller et al., 1969). At atmospheric pressure and 273 K, the calculated ozone diffusion coefficient was 0.22 cm<sup>2</sup> s<sup>-1</sup>. Under most experimental conditions, the radial diffusion correction was negligible for geometric uptake coefficients below 4 × 10<sup>-6</sup> (less than 10% of the experimental value), and it increased progressively with increasing geometric uptake coefficient to a maximum of 50% correction for geometric uptake coefficients of 4 × 10<sup>-5</sup>.

The kinetic parameters were determined after 30 min of exposure to the film. This delay corresponds to the response time of the HCHO analyzer, which is based on the time needed for the HCHO concentration to reach a plateau and at which point the steady-state uptake coefficient ( $\gamma_{\text{ss}}$ ) can be determined. However, kinetics tests performed with an exposure time of 3.5 h showed no HCHO saturation at the TiO<sub>2</sub>-doped surface, suggesting that HCHO uptake was sustained for the entire exposure period.

The experiments were conducted with an HCHO mixing ratio between 3.5 and 32.5 ppbv, a TiO<sub>2</sub> content from 1 to 100 %wt, a film

mass range between 6 and 40 mg and a relative humidity between 6 and 70%.

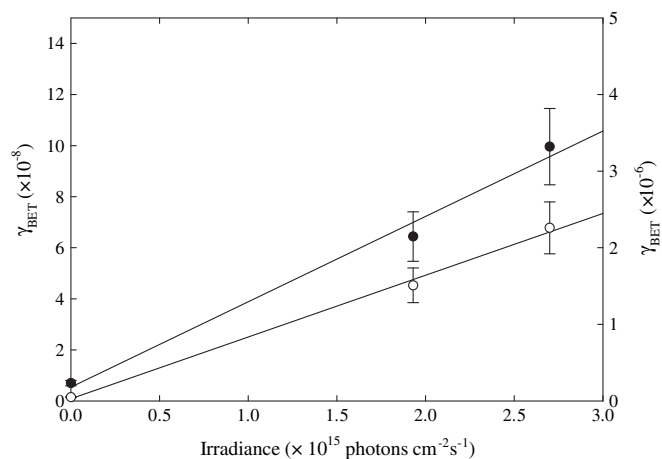
### 3. Results

For all mineral coatings used in this study, the BET uptake coefficients derived from dark experiments were very low (of the order of 3 × 10<sup>-9</sup>). This indicates a weak loss of HCHO on the surface, which is, within our sensitivity, independent of the TiO<sub>2</sub>/SiO<sub>2</sub> mixing ratio.

In the case of pure SiO<sub>2</sub> films, our observations were similar to those of Carlos-Cuellar et al. (2003), who reported low reactivity of HCHO. Under both dark and UV-light conditions, uptake coefficients of (3.1 ± 0.5) × 10<sup>-9</sup> were measured, suggesting that no photoenhancement occurred.

A very different behavior is observed for HCHO uptake onto a TiO<sub>2</sub>-doped surface that is exposed to weak near-UV irradiation (irradiance of 2.7 × 10<sup>15</sup> photons cm<sup>-2</sup> s<sup>-1</sup> in the 340–420 nm range). In this case, the uptake is markedly photoenhanced (nearly 40 times greater than under dark conditions (see Fig. 2)). Under steady-state conditions, these findings underline the importance of photocatalytic HCHO removal at the surface of a film containing traces of TiO<sub>2</sub>. HCHO degradation by photocatalytic engineered systems has been described in the literature (Liu et al., 2005; Obee and Brown, 1995). It is suggested that the photocatalytic oxidation of HCHO is due to surface reaction with OH radicals that are produced from the interaction between adsorbed water and the electron holes that are created when TiO<sub>2</sub> is irradiated with UV light. However, to our knowledge, there are no data available for the HCHO uptake coefficient on irradiated mineral dust films or any proxy of them to be used for atmospheric purposes.

The irradiance used in this study is approximately 5 times less than the solar irradiance between 340 and 420 nm reaching the Earth surface (Gueymard et al., 2002). We therefore investigated the dependence of the BET steady-state uptake coefficient on irradiance under conditions of 293 K, 30% RH and 2 ppbv of HCHO. As shown in Fig. 3, the BET uptake coefficient is linearly dependent on the irradiance, which varied from 1.9 × 10<sup>15</sup> to 2.7 × 10<sup>15</sup> photons cm<sup>-2</sup> s<sup>-1</sup>, thus confirming the heterogeneous photochemical nature of the HCHO loss. If the linearity observed in Fig. 3 is extrapolated to the irradiance reaching the surface of the Earth in the same wavelength range at fixed HCHO mixing ratio and



**Fig. 3.** Dependence of the uptake coefficient as a function of UV light irradiance. Experiments were conducted with 2 ppbv of HCHO at 30% of RH and 293 K. Filled and open circles are raw data carried with 5 %wt of TiO<sub>2</sub> diluted in SiO<sub>2</sub> and pure TiO<sub>2</sub> coatings respectively. The latter data are related to the right hand scale.

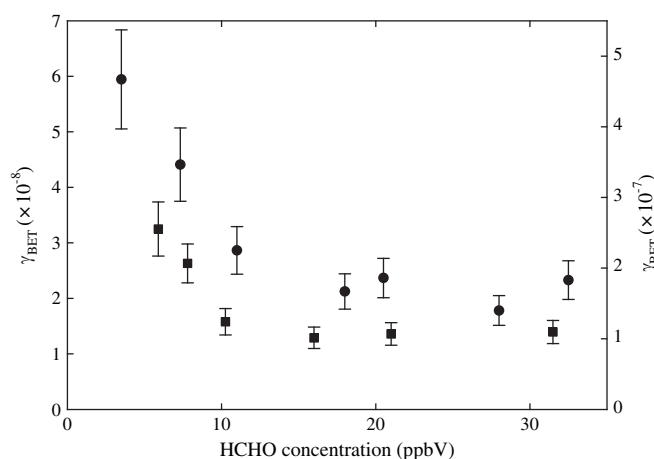
humidity, then it is possible to estimate an atmospherically relevant uptake coefficient. The BET uptake coefficients are normalized to the measured irradiance  $I$  reaching the film during the experiments, according to:

$$\Gamma_{\text{phot}} = \frac{\gamma_{\text{BET}}}{I} \quad (5)$$

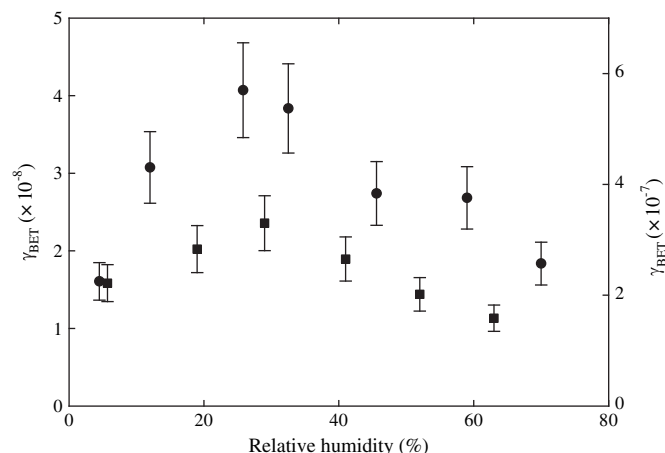
where the obtained normalized coefficient,  $\Gamma_{\text{phot}}$ , has units of  $(\text{mW cm}^{-2})^{-1}$ . For the majority of the experiments,  $I$  was equal to  $1.45 \text{ mW cm}^{-2}$ .  $\Gamma_{\text{phot}}$  can be multiplied by the irradiance reaching the Earth's surface or the troposphere, thus facilitating a rough assessment of the impact of light on the heterogeneous HCHO chemistry on  $\text{SiO}_2$ - $\text{TiO}_2$  oxides, provided that all other parameters are kept constant (see discussion).

Another important atmospheric variable parameter is the initial HCHO mixing ratio. The uptake coefficients were observed to be inversely dependent on the initial gaseous HCHO concentration. Fig. 4 shows the uptake coefficient decreasing from  $(6.0 \pm 0.9) \times 10^{-7}$  to  $(2.0 \pm 0.3) \times 10^{-7}$  for pure  $\text{TiO}_2$  coatings and from  $(3.0 \pm 0.5) \times 10^{-8}$  to  $(1.5 \pm 0.2) \times 10^{-8}$  for 5 %wt  $\text{TiO}_2$  films with increasing HCHO concentration in the range from 3.5 to 32.5 ppbv, with a plateau being attained around 10 ppbv. Our results agree with those reported in many other heterogeneous studies of uptake onto different solid and liquid surfaces, both organic and inorganic (Clifford et al., 2008; Hanisch and Crowley, 2001; Jammoul et al., 2008; McNeill et al., 2007; Mmerekki and Donaldson, 2003; Poeschl et al., 2001). More specifically, the inverse of the uptake rate has been observed to depend linearly with the inverse of the HCHO inlet concentration, in agreement with a Langmuir–Hinshelwood formalism.

The effect of water vapor on the uptake process was also investigated between 6 and 70% relative humidity (RH) for both 5 and 100 %wt of  $\text{TiO}_2$ . As shown in Fig. 5,  $\gamma_{\text{BET}}$  decreases at low (below 20%) and high RH (over 50–60%) and reaches a maximum at approximately 30% RH. This indicates that higher amounts of water inhibit surface loss. Such a dependence on the relative humidity has already been reported (Dibble and Raupp, 1990; Obee and Brown, 1995; Zhang et al., 2006) and can be explained by the competitive adsorption of water and the volatile organic compound (VOC) at the surface as well as the decrease in the amount of OH radicals



**Fig. 4.** Trend of uptake coefficient as a function of the introduced HCHO concentration ranging from 3.5 to 32.5 ppbv. Experiments were performed with 6% of RH, at 293 K in UV-light conditions (lamps irradiance =  $2.7 \times 10^{15} \text{ photons cm}^{-2} \text{ s}^{-1}$ ). Squares (■) and circles (●) correspond to measurements performed with 5 %wt of  $\text{TiO}_2$  diluted in  $\text{SiO}_2$  and pure  $\text{TiO}_2$  coatings respectively. The latter data are related to the right hand scale.

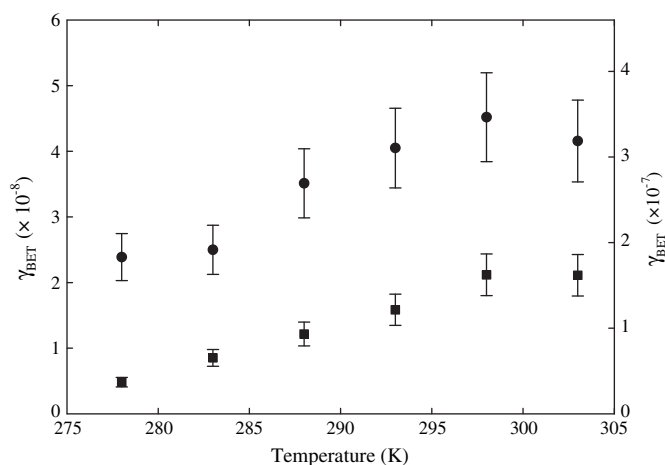


**Fig. 5.** Effect of RH onto uptake coefficients. Experiments were carried out onto illuminated coatings with  $2.7 \times 10^{15} \text{ photons cm}^{-2} \text{ s}^{-1}$  and exposed to 11 ppb of HCHO at 293 K. Squares (■) and circles (●) correspond to measurements performed with 5 %wt of  $\text{TiO}_2$  diluted in  $\text{SiO}_2$  and pure  $\text{TiO}_2$  coatings respectively. The latter data are related to the right hand scale.

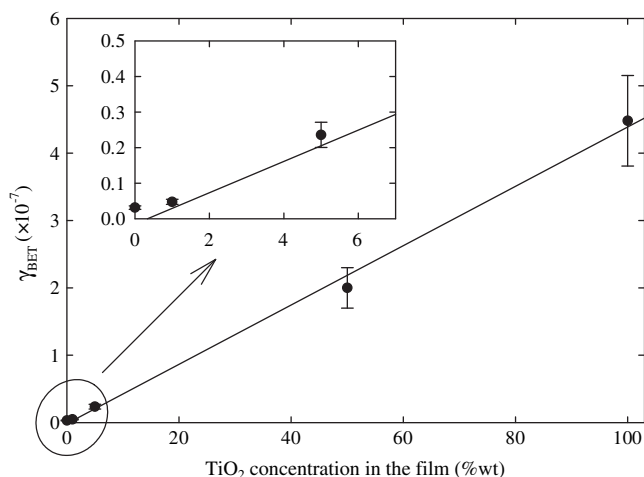
produced at the  $\text{TiO}_2$  surface, which is the driving force for HCHO uptake.

The results shown in Fig. 6 indicate that the HCHO uptake coefficient increases with increasing temperature, which were varied between 278 and 298 K. Specifically, the uptake coefficient increased from  $(1.8 \pm 0.3) \times 10^{-7}$  to  $(3.2 \pm 0.5) \times 10^{-7}$  for pure  $\text{TiO}_2$  coatings and from  $(4.8 \pm 0.8) \times 10^{-9}$  to  $(2.0 \pm 0.3) \times 10^{-8}$  for 5 %wt  $\text{TiO}_2/\text{SiO}_2$  coatings. As adsorption and chemical reactivity have opposite temperature trends, these observations indicate that surface reactions are dominant in the observed positive dependence on the temperature.

In the real environment, exposed surfaces may have variable  $\text{TiO}_2$  content. We therefore tested mixing ratios between 1 and 100 %wt of  $\text{TiO}_2$  in a  $\text{SiO}_2$  matrix and the experimental results are presented in Fig. 7, showing again a linear dependence of the uptake coefficient with respect to the %wt of  $\text{TiO}_2$ .



**Fig. 6.** Effect of Temperature on Uptake coefficient. Experiments were driven with coatings illuminated with  $2.7 \times 10^{15} \text{ photons cm}^{-2} \text{ s}^{-1}$  and exposed to 11 ppb of HCHO at 30% of RH. Squares (■) and circles (●) correspond to measurements performed with 5 %wt of  $\text{TiO}_2$  diluted in  $\text{SiO}_2$  and pure  $\text{TiO}_2$  coatings respectively. The latter data are related to the right hand scale.



**Fig. 7.** Dependence of uptake coefficient with respect to TiO<sub>2</sub> content in the coatings. Experiments were performed with coatings irradiated with  $2.7 \times 10^{15}$  photons  $\text{cm}^{-2} \text{s}^{-1}$  and exhibited to 11 ppb of HCHO at 30% of RH and at 293 K.

#### 4. Discussion and atmospheric implications

The data in this study show a strongly enhanced reactivity of synthetic surfaces containing TiO<sub>2</sub> and SiO<sub>2</sub>, taken as proxies for atmospheric dust particles when irradiated with weak near-UV light using a coated flow tube reactor. Under dark conditions, the steady-state uptake BET coefficient (determined after 30 min of HCHO exposure time to the surface) is estimated as  $(2.97 \pm 0.45) \times 10^{-9}$  onto SiO<sub>2</sub>/TiO<sub>2</sub> (5 %wt) films and  $(3.18 \pm 0.5) \times 10^{-9}$  onto pure TiO<sub>2</sub> coatings. Our results are smaller than those of Xu et al. (2006), who measured  $\gamma_{\text{BET}} = (9.4 \pm 1.7) \times 10^{-9}$  on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> particles at 293 K (Xu et al., 2006). Initial dark uptake kinetics of HCHO onto pure mineral oxide surfaces (i.e., SiO<sub>2</sub>,  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>,  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>) measured by Grassian and co-workers at 295 K in a Knudsen-cell reactor operating at low pressure and under dry conditions (Carlos-Cuellar et al., 2003; Li et al., 2001) were much greater ( $\gamma_{\text{BET}}$  from  $3 \times 10^{-7}$  to  $1 \times 10^{-4}$ ) than our values ( $\gamma_{\text{BET}}$  approx.  $2 \times 10^{-6}$  for pure illuminated TiO<sub>2</sub> coatings). One difference between the two studies is the low time resolution of the present study compared with the quasi-instantaneous response in the molecular flow reactor. Another difference is rapid surface deactivation observed in the Knudsen-cell study, in contrast to the sustained HCHO uptake during the 3.5-h exposure time measured in our work. In fact, water molecules and other trace gases can strongly interact with mineral oxide surfaces affecting the adsorption and reaction kinetics, thereby modifying HCHO uptake onto the surface. Given the atmospheric relevance of the conditions used in the current work, the photo-induced uptake coefficients reported herein may be useful in determining the global impact of mineral aerosol photochemistry in its role as a sink for HCHO in dust plumes. Assessing the global impact of such dust photochemistry is now facilitated by the photoinduced uptake coefficients reported in this study.

The dry deposition of HCHO is generally not considered as an efficient removal pathway. This was confirmed in the current study as the HCHO uptake rate on pure SiO<sub>2</sub> was very slow. However, adding TiO<sub>2</sub> to construction materials may add a new removal pathway close to the ground. The kinetics information obtained in this study can be used to assess whether and under which conditions HCHO removal through TiO<sub>2</sub>-based construction materials may be significant. To do so, we assume an urban area in which TiO<sub>2</sub>-based construction materials are deployed at a large scale, i.e., a city in which buildings are coated with a thin layer of TiO<sub>2</sub>

(as has already been done in some locations). Let us assume that this TiO<sub>2</sub> layer covers between 0% (the case of most current cities) and 100% (a hypothetical futuristic case where all building are constructed using TiO<sub>2</sub>-based construction materials). Using previous modelling studies for dense urban areas (Diamond et al., 2001; Kwamena et al., 2007; Theurer, 1999), which consider both the areas of occupied surface at the ground and shaped constructed surface, we estimate that the building surface exposed to HCHO deposition is 2.25 times the city surface at the ground. Current commercial TiO<sub>2</sub>-based construction materials are covered by an approximately 10-nm-thick active TiO<sub>2</sub> layer (Abdullah et al., 2007) having an internal (BET) surface similar to the films explored in this study. This would expose a chemically active surface with a total area of  $1.04 \times 10^8 \text{ m}^2$  taking into consideration a ground surface of  $46 \times 10^6 \text{ m}^2$  (equivalent to the ground surface of Lyon, France).<sup>1</sup>

To assess if these processes may represent a significant HCHO sink, a simple approach is to compare the lifetimes due to photo-induced uptake on the buildings with those due to the main removal processes, i.e., photolysis or reaction with OH. The lifetimes associated with the main processes are readily available from the literature. Assuming an average OH concentration of  $10^6 \text{ molecules cm}^{-3}$ , the OH channel lifetime is calculated to be almost 26 h (Stief et al., 1980). Given a solar zenith angle of 30° and therefore an irradiance of  $1.92 \times 10^{17} \text{ photons cm}^{-2} \text{ s}^{-1}$  (Calvert, 1980; Finalyson-Pitts and Pitts, 2000), HCHO is photolysed with a lifetime of 6 h. The heterogeneous pathway (i.e., degradation at the surface of TiO<sub>2</sub>-based construction materials) is evaluated using the uptake coefficient derived in this study.

To a first approximation, equation (4) can be used to calculate the HCHO lifetime by replacing the volume of the tube with the volume of air in the urban environment (simply defined as the ground surface times the mixing height) and the surface with the total surface of photocatalytically active material deployed in this virtual city. For these calculations, we used the uptake coefficient measured at 2 ppbv at 30% relative humidity and 293 K. Linear extrapolation of this value to realistic solar conditions ( $I = 1.21 \times 10^{16} \text{ photons cm}^{-2} \text{ s}^{-1}$ ) in the UV region (340–420 nm) gives an estimate of  $(9.7 \pm 1.4) \times 10^{-6}$  for the uptake coefficient onto pure TiO<sub>2</sub> films.

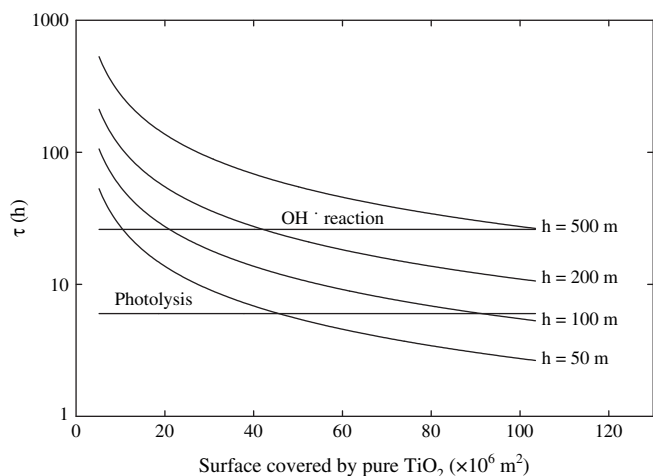
Assuming a mixing height ( $h$ ) between 50 and 500 m, the HCHO lifetime can be approximated as:

$$\tau_d(h) = \frac{5.47 \times 10^6 \times h(\text{m})}{S(\text{m}^2)} \quad (6)$$

Fig. 8 compares all three estimated lifetimes as a function of the urban TiO<sub>2</sub> coverage. From this figure, it is apparent that HCHO loss increases significantly from high to low mixing heights where the deposition process is occurring. Compared to HCHO loss by means of OH<sup>+</sup> reaction, deposition onto urban surfaces from heights ranging from 100 to 200 m is significant if 20 and 40% of the construction surface is covered by pure TiO<sub>2</sub>. Moreover, we note that for the upper mixing heights, HCHO concentrations are estimated to be smaller, which implies faster kinetics deposition, according to Fig. 4. In this case, one may reconsider uptake coefficient values in the calculation of HCHO lifetime.

Hence, for low mixing heights, e.g., 50 m (or, in other words, in close vicinity of buildings), the removal by active depolluting material can compete with other homogeneous removal pathways if 10% or more of the building are covered with TiO<sub>2</sub>. Moreover, if 40% of urban surfaces or more is activated then the heterogeneous removal may dominate over OH reaction and photolysis. Therefore, this hypothetical exercise suggests that implementing TiO<sub>2</sub>-based

<sup>1</sup> [http://www.lyon.fr/vdl/sections/en/vie\\_democratique/institutions/ville\\_lyon\\_1](http://www.lyon.fr/vdl/sections/en/vie_democratique/institutions/ville_lyon_1).



**Fig. 8.** Lifetimes of HCHO due to photolysis, reaction with OH and deposition process onto mineral surfaces. The latter trends are represented as a function of surface covered by TiO<sub>2</sub> coatings for different air mixing heights (ranging from 50 to 500 m).

construction materials can, for the specific case of HCHO, provide an additional sink that could contribute to the improvement of urban air quality.

## 5. Conclusions

This paper describes the kinetics of HCHO loss onto TiO<sub>2</sub>/SiO<sub>2</sub> films to simulate the loss onto mineral aerosol and urban surfaces over atmospherically relevant conditions. The uptake kinetics of the HCHO heterogeneous reaction is explained using a Langmuir-Hinshelwood mechanism.

The measured uptake coefficients were used to estimate the lifetime of HCHO in a city where buildings are treated with TiO<sub>2</sub>-active surfaces. It is estimated that this process may significantly reduce the HCHO level in the direct vicinity of the building surfaces.

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# Nitrogen dioxide removal and nitrous acid formation on titanium oxide surfaces—an air quality remediation process?

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The reactivity of NO<sub>2</sub> on irradiated TiO<sub>2</sub>/SiO<sub>2</sub> films was studied, with different TiO<sub>2</sub> contents, as proxies for NO<sub>x</sub> de-polluting materials. The influence of the photocatalyst concentration, the role of molecular oxygen and the effect of nitrate on the reactivity of TiO<sub>2</sub> films were investigated. NO, HONO and nitrate anions are produced as a consequence of the NO<sub>2</sub> loss on UV-illuminated TiO<sub>2</sub> films. The photoinduced nitrate conversion into NO<sub>x</sub> and HONO at the TiO<sub>2</sub> surface is discussed as being a renoxification process, which involves the NO<sub>3</sub> radical. The presence of O<sub>2</sub> in the carrier gas modifies the NO and HONO production yields in the heterogeneous reaction between NO<sub>2</sub> and TiO<sub>2</sub> as well as the products of the renoxification process. Depending on the nature of the surface, the interaction between NO<sub>2</sub> and nitrate with TiO<sub>2</sub> may generate HONO that may have a negative impact on air quality.

## Introduction

Air pollution originating from traffic is an important problem in most urban areas. Nitrogen oxides (NO<sub>x</sub>), volatile organic compounds (VOCs) and particulate matter (PM) are some of these pollutants. Not only are there strong associations between ambient air pollution levels and adverse health effects<sup>1</sup> but also their transformation within the atmosphere leads to photochemical air pollution.<sup>2</sup> As a result, several regulations have been implemented to reduce emissions from vehicles<sup>3</sup> and also a new approach has been applied in recent years by considering the use of self-cleaning and de-polluting materials to remove these pollutants.<sup>4–7</sup>

Titanium oxide, TiO<sub>2</sub>, has become the material of choice in a variety of remediation processes due to its photocatalytic properties<sup>8,9</sup> and its favourable physical and chemical properties.<sup>9</sup> Besides, it is chemically inert in the dark, not expensive, non toxic and easy to handle. The self-cleaning properties of TiO<sub>2</sub> are ruled by the absorption of band gap light and the production of excited-state conduction-band electrons and valence-band holes, which can react with electron acceptors and electron donors adsorbed on the semiconductor surface.<sup>8</sup> The environmental relevance of TiO<sub>2</sub> is usually related to its overall capacity to deplete organic pollutants from aqueous and gaseous media. Many studies have recently focused on the development of environmentally friendly materials by adding TiO<sub>2</sub> to ordinary building materials such as concrete or by preparing TiO<sub>2</sub> film coatings.<sup>4,5,7,10,11</sup> Although various photocatalytic materials are already on the market, very little reliable information is available, except for limited technical data, regarding their impact on air quality considering the potential formation of harmful intermediates. This scenario motivates further studies in the field.<sup>11</sup>

Different works were focused on achieving the removal of NO<sub>x</sub> from air by means of de-polluting surfaces containing TiO<sub>2</sub>.<sup>4,7,12–23</sup> However, recent studies showed that UV-illuminated surfaces of pure TiO<sub>2</sub> aerosols can reduce NO<sub>2</sub> to HONO, together with the production of H<sub>2</sub>O<sub>2</sub>.<sup>24,25</sup> Besides the important impact of nitrous acid (HONO) as a free radical source in the atmosphere,<sup>26</sup> there are several mechanisms by which HONO may be harmful to health. Firstly, HONO is an acid, which may damage mucous membranes and surfaces of the respiratory tract. Secondly, in the reaction of HONO with amino groups of the nucleotides, the double helix of the DNA can be cross-linked<sup>27–31</sup> leading to mutagenic properties. In addition, in the reaction of HONO with amines, both in the atmosphere but also *in vivo*, nitrosamines are formed<sup>32–35</sup> which show carcinogenic and mutagenic properties.<sup>36,37</sup> Langridge *et al.* have just reported the formation of nitrous acid on a self-cleaning window glass coated by TiO<sub>2</sub>.<sup>38</sup> In addition, the photoenhanced NO<sub>2</sub> uptake for real mineral dusts with HONO production was assigned to the chemistry occurring on the TiO<sub>2</sub>.<sup>39,40</sup> In this process, nitrate anions are formed as a consequence of the photocatalytic oxidation of NO<sub>2</sub> on UV-illuminated TiO<sub>2</sub> surfaces.<sup>16,24,41–44</sup> Most of these studies argue that nitrate is the innocuous final product of the photocatalytic NO<sub>x</sub> removal process. However, the photochemistry of nitrate doped mineral dust samples containing TiO<sub>2</sub> was proved to be a potential renoxification process of the atmosphere.<sup>45</sup> In addition, the photochemistry of adsorbed nitrate on aluminium oxide has been proved to give different yields of NO, NO<sub>2</sub> and N<sub>2</sub>O according to the presence of water and molecular oxygen.<sup>46,47</sup>

In this study, we investigated the reactivity of irradiated TiO<sub>2</sub>/SiO<sub>2</sub> films with different TiO<sub>2</sub> contents as proxies for de-polluting materials towards NO<sub>2</sub>. The influence of the photocatalyst concentration was evaluated on the heterogeneous reaction with NO<sub>2</sub> using either pure N<sub>2</sub> or a mixture of O<sub>2</sub> (15%) and N<sub>2</sub> (85%) as carrier gases. The role of O<sub>2</sub> in the gas phase product distribution as well as the influence of nitrate on the reactivity of TiO<sub>2</sub> films were investigated. It was found that

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O<sub>2</sub> plays a critical role in NO and HONO formation as well as on the products of the renoxification process that occurs on the TiO<sub>2</sub> films prepared with nitrate. A possible reaction mechanism is proposed to explain the results obtained.

## Experimental

### Samples

SiO<sub>2</sub> (Aerosil 130, Degussa) and TiO<sub>2</sub> powders (80% anatase, 20% rutile; Degussa P25) were used as purchased. A total mass of 2 g of TiO<sub>2</sub> and SiO<sub>2</sub> powder was dissolved in 20 ml of water. Different TiO<sub>2</sub> (x%)/SiO<sub>2</sub> films were prepared, varying the percentage between 10 and 100. This suspension was dripped uniformly into a Pyrex tube (20 cm length, 1.1 cm i.d.) and dried overnight in an oven at 100 °C. The resulting homogeneous film covered the entire inner area of the tube and was uniform in thickness.<sup>48</sup>

### Flow reactor

The uptake experiments were conducted in a horizontal cylindrical coated-wall flow tube reactor made of Pyrex. The Pyrex tube containing the TiO<sub>2</sub>/SiO<sub>2</sub> film was placed in the reactor, which was surrounded by 3 fluorescent lamps (OSRAM Sylvania TLD15W/08) with a continuous emission in the 340–420 nm range with a total irradiance of  $1.5 \times 10^{15}$  photons cm<sup>2</sup> s<sup>-1</sup>. The spectral irradiance for the UV lamps reaching the inner surface of the reactor and its uniformity has been quantified using two methods as described by Jammoul *et al.*<sup>49</sup> NO<sub>2</sub> was introduced in the flow tube by means of a movable injector with radius 0.3 cm. Synthetic air as well as pure nitrogen were used as carrier gases with a total flow rate of 200 sccm in the flow tube reactor, ensuring a laminar regime. The NO<sub>2</sub> and NO concentrations were measured at the reactor exit as a function of the injector position along the tube. This position determined the exposure time of the film surface towards the gas. A THERMO 42C chemiluminescent analyzer was used for NO and NO<sub>2</sub> detection. The latter is based on the reaction between NO and O<sub>3</sub>, which produces a characteristic luminescence with an intensity that is linearly proportional to the NO concentration. NO<sub>2</sub> is transformed into NO by means of a molybdenum converter in order to be measured with the chemiluminescent reaction. As HONO is detected by the instrument as NO<sub>2</sub>, a denuder tube (9 cm × 0.95 cm i.d.) containing a mixture of K<sub>2</sub>CO<sub>3</sub>/Na<sub>2</sub>CO<sub>3</sub> (Fluka) was introduced between the exit of the flow cell reactor and the detector. The denuder was either bypassed, leading to the detection of NO and NO<sub>2</sub> together with HONO; or it was switched into the sample line along the experiment, so that only NO and NO<sub>2</sub> species were measured after HONO removal from the gas stream. Therefore, HONO concentration was obtained as the difference of the detector signal without and with the carbonate denuder in the sampling line.<sup>50</sup>

Gas phase NO<sub>2</sub> concentration used in the experiments was fixed at 150 ppbv ( $3.8 \times 10^{12}$  molecules cm<sup>-3</sup>). The experiments were conducted at  $298 \pm 1$  K by circulating temperature-controlled water through the outer jacket of the flow tube reactor and were performed under atmospheric pressure and 30% relative humidity. The temperature of the gas streams

and the humidity were measured by using an SP UFT75 sensor (Partners BV). All gases were taken directly from cylinders without further purification prior to use. High purity synthetic air (99.999%), N<sub>2</sub> (99.0%) and NO<sub>2</sub> (1 ppmv in N<sub>2</sub>; 99.0%) were purchased from Air Liquide. The gas flows were monitored before entering the reactor by mass flow controllers (Brooks).

Periodical calibrations of the NO<sub>2</sub> from the bottle were performed using the carbonate denuder. Only 3% of the total NO<sub>2</sub> (and possible contaminants) was trapped in the denuder. This value was then considered in the calculation of the uptake coefficients and product yields.

NO<sub>2</sub> photodissociates with unit quantum yield in the wavelength region emitted by the lamps (340–420 nm), but its loss in the gas phase is negligible for the residence time of 6 s used in our experiments. An estimation of the photolysis rate constant,  $J = 4.75 \times 10^{-4}$  s<sup>-1</sup> gives rise to a loss of 0.3% of the total NO<sub>2</sub> (g). Control experiments were performed to confirm the chemical inactivity of the Pyrex flow tube surfaces, and to evaluate the contribution of NO<sub>2</sub> photolysis. The empty tube (with no film) was filled with NO<sub>2</sub> and exposed to light. NO<sub>2</sub> photodissociation and loss at the Pyrex surface were negligible (below 3% of the total NO<sub>2</sub> loss) in comparison to the NO<sub>2</sub> loss observed in the presence of the TiO<sub>2</sub>/SiO<sub>2</sub> film.

### Uptake coefficient

The kinetic behaviour of the heterogeneous reaction between NO<sub>2</sub> and TiO<sub>2</sub>/SiO<sub>2</sub> films under irradiation can be well described by assuming a pseudo first-order reaction with respect to the gas-phase NO<sub>2</sub> concentration. The derived first-order rate constant,  $k_{\text{obs}}$ , is related to the geometric uptake coefficient ( $\gamma_{\text{g}}$ ) by:

$$\frac{d}{dt} \ln \frac{C_0}{C_i} = k_{\text{obs}} = \frac{\gamma_{\text{g}} \langle c_{\text{NO}_2} \rangle}{2r_{\text{tube}}} \quad (1)$$

where  $r_{\text{tube}}$ ,  $\gamma_{\text{g}}$ ,  $t$ , and  $\langle c_{\text{NO}_2} \rangle$  are the flow-tube radius (0.547 cm), the geometric uptake coefficient, the exposure time, and the NO<sub>2</sub> average molecular velocity, respectively.  $C_0$  is the NO<sub>2</sub> concentration when there is no contact between the film and the reagent; whereas  $C_i$  is the trace gas concentration when the contact with NO<sub>2</sub> is allowed. The uptake coefficient is defined as the fraction of effective collisions between a gas phase reagent and a reactive surface that lead to the loss of the gas phase reagent due to chemical reaction.  $\gamma_{\text{g}}$  is a mass dependent parameter for these substrates as diffusion and reaction of the trace gas take place at the internal surface of the films.<sup>42</sup> For that reason, a mass-independent uptake was derived by taking into account the entire BET surface area of the TiO<sub>2</sub>/SiO<sub>2</sub> films.<sup>39,51</sup>

All experiments have been duplicated. The errors related to replicates are smaller than those associated with the variables involved in the calculation of  $\gamma$ .

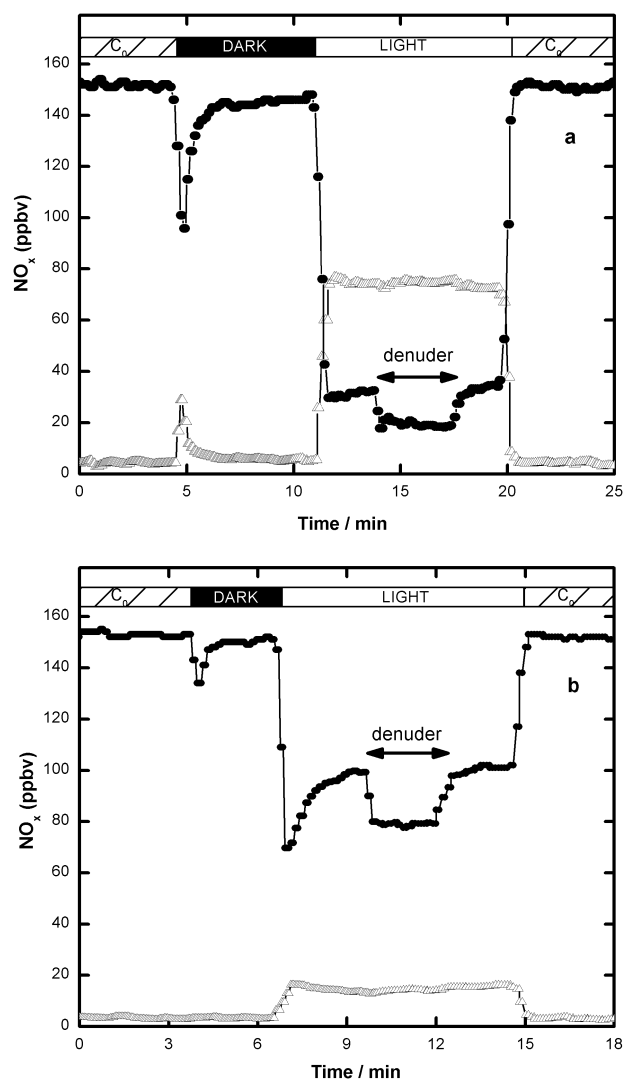
Eqn (1) does not contemplate possible diffusion limitations caused by the formation of a radial concentration gradient in the gas phase, which would occur if the loss at the surface is too fast to be recovered with the reagent supply. As a consequence, the uptake coefficient was calculated by using

the Cooney-Kim-Davis (CKD) method,<sup>52</sup> which takes into account axial and lateral diffusion combined with a first order loss at the inner surface of a cylindrical tube under laminar flow conditions. An implementation of this method has been previously used.<sup>53</sup> The diffusion coefficient,  $D$ , was calculated using the formula proposed by Fuller *et al.*<sup>54</sup>

## Results and discussions

Fig. 1 illustrates the behaviour of TiO<sub>2</sub> (10%)/SiO<sub>2</sub> films exposed to a continuous flow of 150 ppbv of NO<sub>2</sub> in the dark and under irradiation for a fixed length of the flow tube. Fig. 1a and b show the results obtained in pure N<sub>2</sub> and in the mixture of O<sub>2</sub> and N<sub>2</sub>, respectively. An NO<sub>2</sub> concentration of 150 ppbv was chosen for these studies because it is representative of NO<sub>2</sub> concentrations found during intense photochemical pollution events in urban environments.<sup>24,55</sup> In addition, it allowed varying the TiO<sub>2</sub> content from 10 to 100% (as the observed rate is slower at higher gas phase concentrations). Once a constant initial NO<sub>2</sub> concentration was established, the injector was withdrawn to a certain distance to expose some fraction of the film to NO<sub>2</sub>, indicated in the top of the figure with a black bar. The NO<sub>2</sub> was allowed to stabilize until it reached a plateau, returning to its initial concentration. The uptake in the dark was more important in absence of O<sub>2</sub> in the carrier gas for all residence times and for films with 10% and 100% of TiO<sub>2</sub>. This behaviour may be related to the competition between NO<sub>2</sub> and O<sub>2</sub> for the adsorption sites on the film surface. When the lamps were turned on, a strong decrease of the NO<sub>2</sub> signal was observed (it must be remembered that without the alkaline denuder this signal corresponds to the sum of the NO<sub>2</sub> and HONO species) highlighting a light induced effective uptake on these surfaces introduced by a fast chemical reaction. The production of HONO was then verified under both conditions by passing the sample line through an alkaline denuder which trapped acidic species before detection. NO was produced both in absence and presence of O<sub>2</sub> in the carrier gas, the latter being in agreement with previous results.<sup>44</sup> When the lamps were turned off and the injector was moved forward to its original position, the NO<sub>2</sub> concentration returned to the initial value. Fig. 1 clearly shows that the NO<sub>2</sub> uptake on the samples, as well as the NO and HONO formation, were considerably enhanced under irradiation, both in the presence and absence of molecular oxygen in the carrier gas for films with 10 wt% TiO<sub>2</sub>. The HONO yield was higher in presence of O<sub>2</sub> whereas the NO formation was favoured in the absence of O<sub>2</sub> (see Table 1).

The analytical procedure used here is not specific to HONO as the alkaline trap inserted periodically in front of the NO<sub>x</sub> analyzer would trap any acidic gases. Therefore, only indirect detection of the produced HONO was made here by means of a NO/NO<sub>x</sub> chemiluminescence detector, in combination with a sodium carbonate denuder tube for removing HONO from the gas stream. However, a direct HONO detection was made by using the HONO specific LOPAP device (long path absorption photometer) in a previous study on TiO<sub>2</sub> surfaces.<sup>39</sup> This product identification has also been independently confirmed by other studies also involving TiO<sub>2</sub> surfaces and different analytical devices.<sup>25,38</sup> We are therefore highly confident that



**Fig. 1** NO<sub>2</sub> loss under irradiation of a TiO<sub>2</sub> (10%)/SiO<sub>2</sub> film when (a) only N<sub>2</sub> was used as carrier gas, and (b) when the O<sub>2</sub> (15%)/N<sub>2</sub> (85%) mixture was used as carrier gas. (●): NO<sub>2</sub> signal; (△): NO signal. The dashed bars correspond to the initial concentration of NO<sub>2</sub> which is not in contact with the film. The black and the white bars indicate the contact time between the NO<sub>2</sub> flow and a certain length of the film in the dark and under irradiation, respectively. The inclusion of the denuder into the sample line is indicated in the figure (see Experimental).

the gaseous species escaping these surfaces is HONO (nitric acid would be trapped much more efficiently on the surface).

Regarding the heterogeneous reaction on irradiated 100% TiO<sub>2</sub> films, NO was only detected in absence of O<sub>2</sub> whereas HONO was mainly formed when O<sub>2</sub> was present in the carrier gas (Table 1). Indeed, the uptake coefficients ( $\gamma_{\text{BET}}$ ) obtained for the NO<sub>2</sub> loss under irradiation were highly influenced by the presence of O<sub>2</sub>, being one order of magnitude higher in pure N<sub>2</sub> for 100 wt% TiO<sub>2</sub> and two orders higher for the film prepared with 10 wt% TiO<sub>2</sub>. This result suggests a competition between O<sub>2</sub> and NO<sub>2</sub> for scavenging the electrons at the surface of the photocatalyst.

The effect of the TiO<sub>2</sub> content on the NO<sub>2</sub> loss was determined for illuminated TiO<sub>2</sub>/SiO<sub>2</sub> films (Fig. 2). As

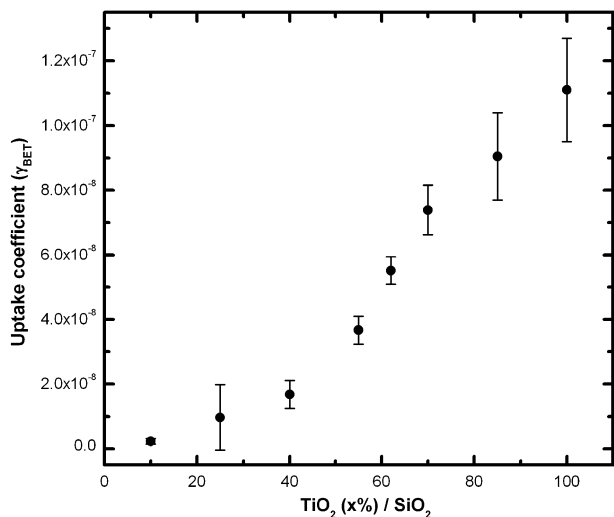
**Table 1** Effect of the carrier on the uptake coefficients, HONO and NO yields when exposing the films to 150 ppbv of NO<sub>2</sub>. Errors are 2σ precision

Carrier	TiO <sub>2</sub> (x%)/SiO <sub>2</sub>	γ <sub>BET</sub>	HONO (%)	NO (%)
N <sub>2</sub>	10	(2.0 ± 0.6) × 10 <sup>-7</sup>	8 ± 2	50 ± 10
O <sub>2</sub> (15%)/N <sub>2</sub> (85%)	10	(2.2 ± 0.8) × 10 <sup>-9</sup>	14 ± 4	26 ± 8
N <sub>2</sub>	100	(1.5 ± 0.4) × 10 <sup>-6</sup>	3 ± 1	71 ± 8
O <sub>2</sub> (15%)/N <sub>2</sub> (85%)	100	(1.1 ± 0.2) × 10 <sup>-7</sup>	12 ± 4	—

expected, the uptake coefficients increased with increasing TiO<sub>2</sub> content in the films, which *a priori* would indicate that the higher the content of TiO<sub>2</sub> at the surface, the more efficient it should be as a de-polluting material.<sup>4</sup> As shown in Table 2 HONO was produced for all TiO<sub>2</sub> concentrations tested under irradiation, while NO was produced only on films containing between 10 and 55% of TiO<sub>2</sub>. Furthermore, the HONO + NO yields on the different TiO<sub>2</sub>/SiO<sub>2</sub> films were always lower than 100%. This result may be explained by the formation of nitrate during the heterogeneous reaction between TiO<sub>2</sub> and NO<sub>2</sub> under irradiation.<sup>16,24,41–44</sup> Rodriguez *et al.*<sup>56</sup> have proved by photoemission data and DF (density functional) calculations that surface NO<sub>3</sub> is formed through the disproportionation of NO<sub>2</sub> on Ti sites.

The influences of humidity and photon flux were reported previously<sup>39</sup> and were not repeated here as the high content of TiO<sub>2</sub> does not allow the use of a wide range of irradiance in our particular experimental set up in order to prevent the kinetics from being limited by the rate of gas phase diffusion, conditions in which heterogeneous kinetics cannot be measured.

After exposure to NO<sub>2</sub> under irradiation the films were flushed by a constant flow of synthetic air or pure N<sub>2</sub> (depending on the carrier gas used in each case) in order to promote molecule desorption from the surface. Once no further traces of NO and NO<sub>2</sub> were observed, lamps were turned on again and emission of nitrogen containing species from the surface was observed. Fig. 3 shows the formation of NO and NO<sub>2</sub> under irradiation for both carrier gases.



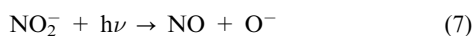
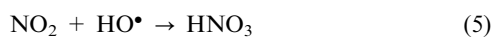
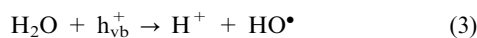
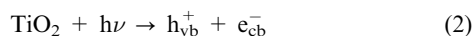
**Fig. 2** Effect of TiO<sub>2</sub> content on the uptake coefficient when the films were exposed to 155 ppbv of gas phase NO<sub>2</sub> under irradiation using O<sub>2</sub> (15%) and N<sub>2</sub> (85%) as carrier. Error bars are 2σ precision.

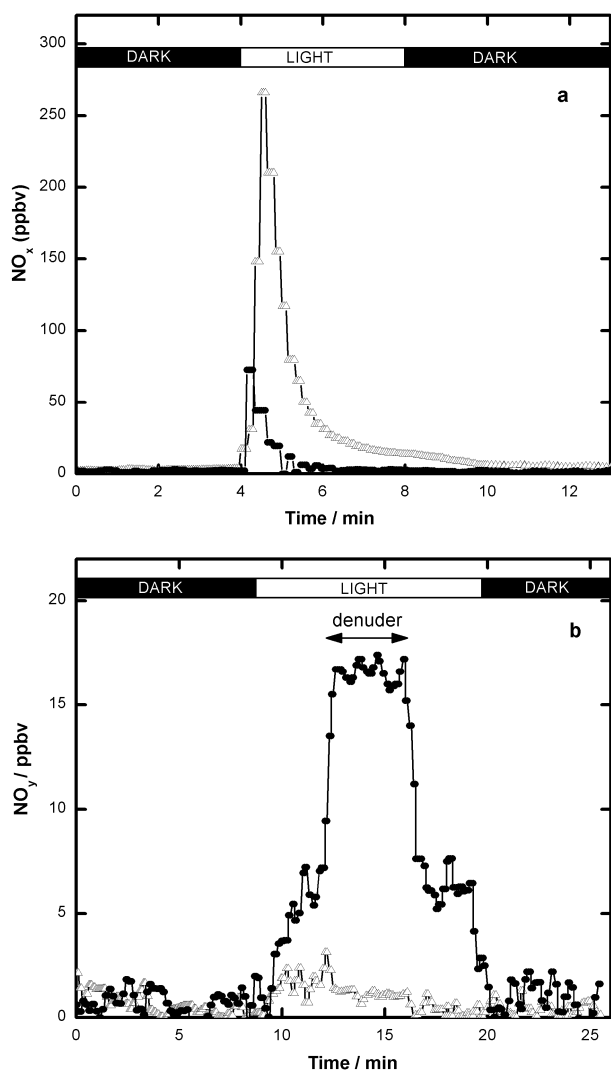
**Table 2** Effect of the TiO<sub>2</sub> content on the gas phase product yields when exposing the films to 150 ppbv of NO<sub>2</sub> under irradiation using O<sub>2</sub> (15%) and N<sub>2</sub> (85%) as carrier. Errors are 2σ precision

TiO <sub>2</sub> (x%)/SiO <sub>2</sub>	HONO (%)	NO (%)
10	14 ± 4	26 ± 8
25	35 ± 2	16 ± 4
40	28 ± 7	42 ± 9
55	36 ± 20	49 ± 20
62	11 ± 5	3 ± 1
70	10 ± 6	2 ± 1
85	27 ± 7	—
100	12 ± 4	—

In agreement with the results presented in Fig. 1, NO was the major product in pure nitrogen (Fig. 3a). However, not only was NO<sub>2</sub> the major product when air was used as carrier gas, but also the production of another volatile compound was observed when passing the effluent flow through the carbonate denuder (Fig. 3b). This product was observed for films which had previously been exposed to NO<sub>2</sub> under illumination and contained between 40 and 100% TiO<sub>2</sub>, and it was not observed when N<sub>2</sub> was used as carrier gas. We hypothesise that the signal observed when switching the carbonate denuder into the sample line may be due to N<sub>2</sub>O formation, as previously observed by Rubasinghe and Grassian on aluminium oxide particle surfaces containing adsorbed nitrate.<sup>46</sup> While this is speculative, as our analytical system is not specific nor sensitive to N<sub>2</sub>O, our results clearly suggest that nitrate ions produced during the heterogeneous reaction of NO<sub>2</sub> and illuminated TiO<sub>2</sub> films may be involved in a renoxification process (*i.e.* production of NO<sub>x</sub> from reservoir compounds believed to be unreactive, such as the nitrate anions) as previously discussed by Ndour *et al.* for mineral dusts containing TiO<sub>2</sub>.<sup>45</sup> The yield of NO (as shown in Fig. 3a) from an irradiated surface, previously exposed to 150 ppbv of NO<sub>2</sub> in N<sub>2</sub>, is 20% of the nitrate produced on this surface and the yield of NO<sub>2</sub> is *ca.* 4%. In other words, 20–25% of nitrate anions deposited on these surfaces may be reprocessed into gaseous NO<sub>x</sub>.

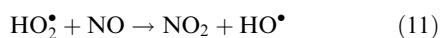
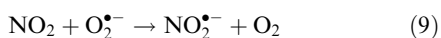
The proposed mechanism for the obtained gas phase products, which is consistent with that reported by Ohko *et al.*<sup>44</sup> is the following:





**Fig. 3** Effect of light on pure TiO<sub>2</sub> films which were previously exposed to NO<sub>2</sub> and light using (a): N<sub>2</sub> as carrier gas; and (b): synthetic air as carrier gas. The black and the white bars indicate the contact time between the carrier flow and the total length of the film in the dark and under irradiation, respectively. The inclusion of the denuder into the sample line is indicated in the figure. (●): NO<sub>2</sub> signal; (Δ): NO signal.

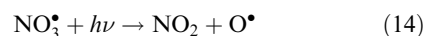
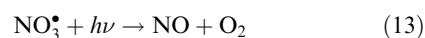
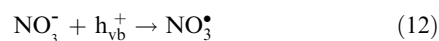
In the presence of molecular oxygen, there is an electron transfer to O<sub>2</sub> that acts as the primary electron acceptor, leading to oxygen activated species<sup>8,57,58</sup> which can participate in the previous mechanism as follows:



These pathways explain the higher HONO yield and the lower NO yield obtained from the heterogeneous reaction between NO<sub>2</sub> and illuminated TiO<sub>2</sub> films when O<sub>2</sub> is present in the

carrier gas. The production of HO<sub>2</sub><sup>•</sup> by reaction (10) leads to the formation of H<sub>2</sub>O<sub>2</sub>, which has been observed by Beaumont *et al.*<sup>24</sup> Indeed, no H<sub>2</sub>O<sub>2</sub> is detected in absence of O<sub>2</sub>.<sup>8</sup> Gerischer and Heller<sup>59</sup> have suggested that electron transfer to O<sub>2</sub> may be the rate-limiting step in semiconductor photocatalysis. Hirakawa *et al.* have proved that O<sub>2</sub><sup>• -</sup> participates in the decomposition of alcohols.<sup>60</sup>

A second set of experiments was performed to verify the role of nitrate anions in the renoxification process, using TiO<sub>2</sub> films prepared with 50 wt% of KNO<sub>3</sub>. Again, the role of molecular oxygen in the carrier gas was investigated. Fig. 4a shows that NO was the major product when pure N<sub>2</sub> was used as carrier gas, in agreement with the results from Fig. 3a, while NO<sub>2</sub> and HONO were the main products in the presence of the carrier gas with O<sub>2</sub>. Similarly, Schuttelfield *et al.*<sup>47</sup> observed high NO<sub>2</sub> and low NO emission during the renoxification process of nitrate adsorbed on alumina surfaces in an atmosphere with oxygen. Rubasinghege and Grassian<sup>46</sup> suggested that oxygen vacancy sites may play a role in the photochemical process of adsorbed nitrate or on the chemistry of the photoproducts, as these sites may be binding sites for molecular O<sub>2</sub>. Fig. 4 also shows that NO release in pure N<sub>2</sub> is faster than the release of NO<sub>2</sub> in air, which is also in agreement with the results shown in Fig. 3. This difference can also be explained considering the affinity of O<sub>2</sub> for the adsorption sites of TiO<sub>2</sub>. Control experiments were carried out to determine whether nitrate photolysis was involved in the release of NO, HONO and NO<sub>2</sub>. None of these products were observed on films without TiO<sub>2</sub>; indeed irradiation of a SiO<sub>2</sub>/KNO<sub>3</sub> 50 wt% and KNO<sub>3</sub> film did not lead to any NO<sub>y</sub> release, at least over our limit of detection. These control experiments indicate that nitrate photolysis was a negligible pathway in our experiments, in contrast to the mechanism proposed by Grassian and co-workers<sup>46,47</sup> on adsorbed nitrate on aluminium oxide particles. The proposed mechanism for the renoxification process has already been discussed by Ndour *et al.*<sup>45</sup> for dust samples irradiated in pure N<sub>2</sub>.



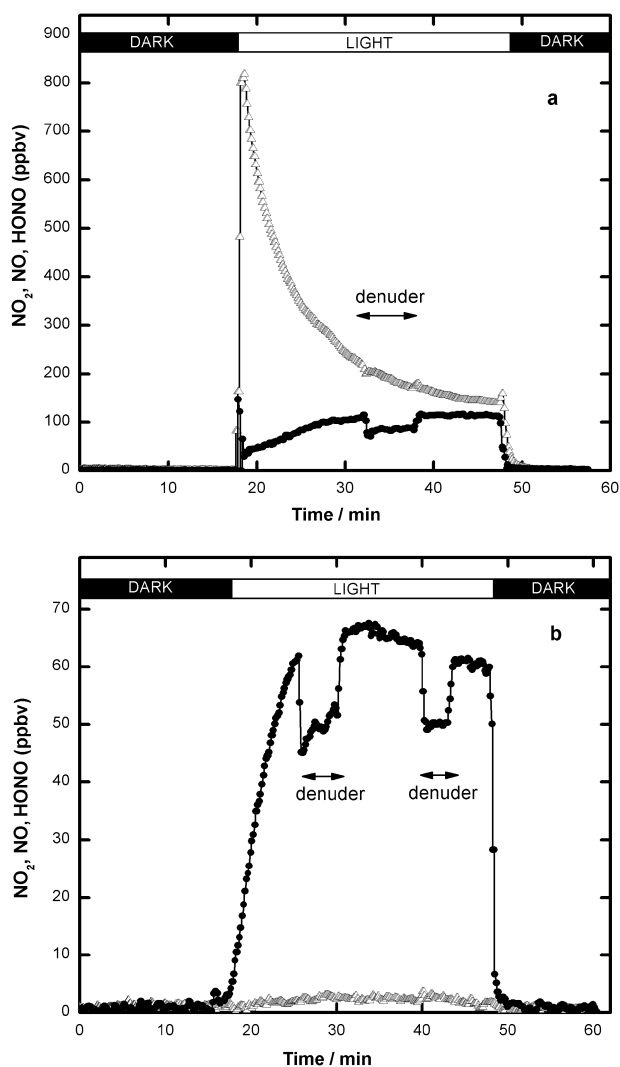
The ability of a TiO<sub>2</sub>/KNO<sub>3</sub> 50 wt% film to remove NO<sub>2</sub> (~170 ppbv) under irradiation in an atmosphere with O<sub>2</sub> was also investigated. Fig. 5 shows that the TiO<sub>2</sub> surface is active towards NO<sub>2</sub> removal with HONO production under irradiation even when the film was prepared with a high content of nitrate. The observed NO<sub>2</sub> loss (~35 ppbv) approximately balances the release of NO<sub>2</sub> (~50 ppbv) from the renoxification process (Fig. 4b) and the NO<sub>2</sub> loss (~85 ppbv) observed on a film of TiO<sub>2</sub> (55%)/SiO<sub>2</sub>, shown in Fig. 6. These results are in disagreement with previous studies,<sup>43,44</sup> where the photocatalyst was deactivated by the nitrate ions produced during the photo-oxidation. But these previous investigations did not consider the renoxification process occurring at the surface of the TiO<sub>2</sub> film when nitrate ions are deposited. This result suggests that HONO would not only be produced during the heterogeneous

reaction between  $\text{NO}_2$  and a clean irradiated  $\text{TiO}_2$  surface, but also on a  $\text{TiO}_2$  surface containing nitrate. As a consequence, special care should be taken in the development of an environmentally friendly material which contains  $\text{TiO}_2$  in its matrix as undesired products may also be formed under irradiation.

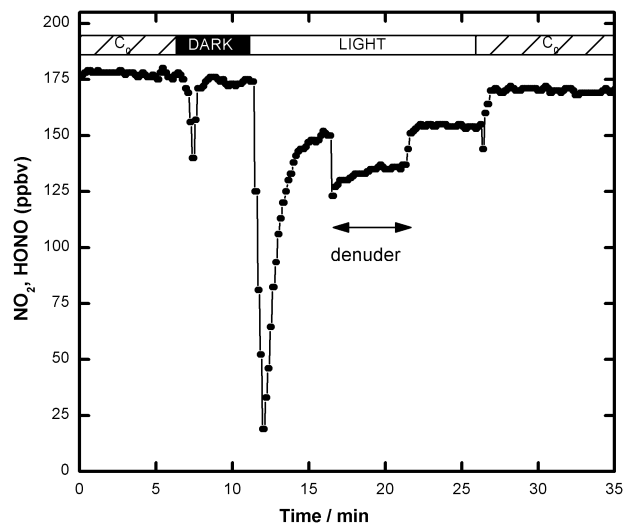
## Conclusions

The present paper suggests that de-polluting materials based on  $\text{TiO}_2$  may contribute to the production of HONO, NO and  $\text{NO}_2$ . The NO, HONO and nitrate are produced as a consequence of the uptake of  $\text{NO}_2$  on UV-illuminated  $\text{TiO}_2$  films.

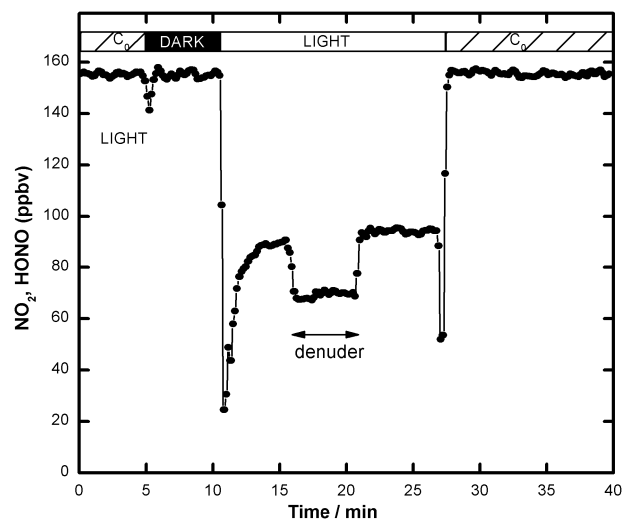
The presence of  $\text{O}_2$  in the carrier gas modifies the NO and HONO production yields in the heterogeneous reaction



**Fig. 4** Effect of light on a  $\text{TiO}_2/\text{KNO}_3$  50 wt% film when (a): it is exposed to a flow of  $\text{N}_2$ ; and (b): it is exposed to a flow of synthetic air. The black and the white bars indicate the contact time between the carrier flow and the film in the dark and under irradiation, respectively. The inclusion of the denuder into the sample line is indicated in the figure. (●):  $\text{NO}_2$  signal; (Δ): NO signal.



**Fig. 5** Effect of the  $\text{NO}_2$  exposure under irradiation after the renoxification process on the same film of  $\text{TiO}_2/\text{KNO}_3$  50 wt% presented in Fig. 4b. The dashed bars correspond to the initial concentration of  $\text{NO}_2$  which is not in contact with the film. The black and the white bars indicate the contact time between the  $\text{NO}_2$  flow and the film in the dark and under irradiation, respectively. (●):  $\text{NO}_2$  signal.



**Fig. 6** Effect of the  $\text{NO}_2$  exposure under irradiation on a film of  $\text{TiO}_2$  (55%)/ $\text{SiO}_2$ . The dashed bars correspond to the initial concentration of  $\text{NO}_2$  which is not in contact with the film. The black and the white bars indicate the contact time between the  $\text{NO}_2$  flow and the film in the dark and under irradiation, respectively. (●):  $\text{NO}_2$  signal.

between  $\text{NO}_2$  and  $\text{TiO}_2$ . NO was the major product in an  $\text{O}_2$  free atmosphere, whereas HONO formation was favoured in the presence of  $\text{O}_2$ . This difference can be elucidated by the presence of activated oxygen species, such as  $\text{O}_2^{\bullet-}$  and  $\text{HO}_2^{\bullet}$ , in the reaction mechanisms.

A renoxification pathway that involves the photochemistry of the  $\text{NO}_3$  radical leads to the release of NO,  $\text{NO}_2$  and of HONO from the  $\text{TiO}_2$  surface. The gas phase product distribution depends on the carrier gas used, in agreement with the uptake experiments.

The renoxification process carried out on the surface of TiO<sub>2</sub> containing materials questions their use for the improvement of air quality as it has been recently suggested. In the real atmosphere, different organic and inorganic compounds may compete for the TiO<sub>2</sub> sites and may be involved in different reactions, which may modify the product yields presented in this work. These processes need to be considered further as potentially important in polluted urban atmospheres, taking into account the role of buildings, roads and natural materials in promoting heterogeneous reactions.<sup>61</sup>

Consequently, these results suggest the need for field measurements of NO<sub>x</sub> levels in locations where self-cleaning materials are already being used, as well as the need for further basic investigation into these new materials.

## Acknowledgements

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## Ozone Formation from Illuminated Titanium Dioxide Surfaces

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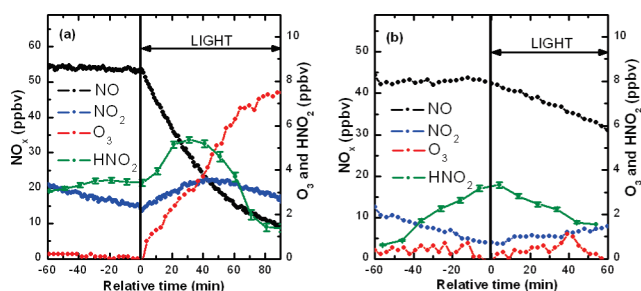
Titanium dioxide, TiO<sub>2</sub>, is used in a variety of remediation processes due to its favorable physical, chemical, and photocatalytic properties.<sup>1–3</sup> Possible removal of NO<sub>x</sub> by means of depolluting surfaces containing TiO<sub>2</sub> has been previously reported.<sup>4–13</sup> Other recent studies<sup>14–17</sup> show that this process converts NO<sub>2</sub> to HNO<sub>2</sub> producing also H<sub>2</sub>O<sub>2</sub><sup>18</sup> and nitrate anions<sup>9,18–22</sup> which are then involved in a renoxification process.<sup>23</sup> Similarly, the photochemistry of adsorbed nitrate on aluminum oxide has been proven to produce NO, NO<sub>2</sub>, and N<sub>2</sub>O.<sup>24,25</sup> However, the formation of non-nitrogen containing products in the NO<sub>x</sub> reaction with illuminated TiO<sub>2</sub> surfaces has been largely unexplored.

Herein, we report the first investigation of such products from TiO<sub>2</sub> coated glasses exposed to nitrogen oxides (NO<sub>x</sub>) in two simulation chambers using both artificial and natural illumination and from irradiated TiO<sub>2</sub>/KNO<sub>3</sub> films using a coated-wall flow tube reactor. These studies demonstrate the formation of ozone from TiO<sub>2</sub> surfaces containing nitrate anions.

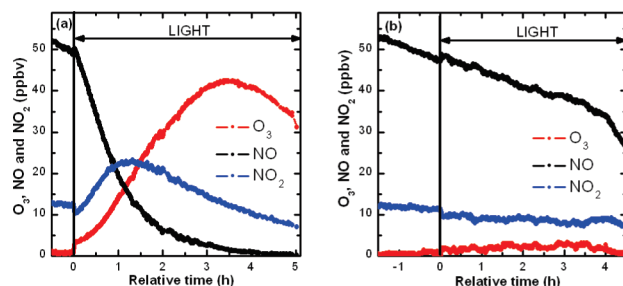
Chamber simulation experiments are performed in two different chambers (i) a stainless steel Multiphase Atmospheric Experimental Simulation Chamber (CESAM) equipped with artificial irradiation and (ii) a Teflon outdoor chamber (see Supporting Information for experimental details and Figures S1–S3). After introduction of synthetic air and NO into the CESAM chamber, the concentrations of NO, NO<sub>2</sub>, HNO<sub>2</sub>, and O<sub>3</sub> are monitored in the dark for 1 h. Then, the artificial illumination is turned on, and the gas mixture is again monitored for typically 90 min.

A similar procedure is adopted for the experiments conducted in the Teflon outdoor chamber using natural illumination. In the latter, known amounts of NO and NO<sub>2</sub> are injected after flushing with dry purified air, and the NO, NO<sub>2</sub>, and O<sub>3</sub> concentrations are monitored for 30 min in the dark. The reactor is then exposed to natural light, and the gas mixture composition is monitored for 4 h. The results for a TiO<sub>2</sub> coated glass and for a standard glass studied with the CESAM and the outdoor chamber are displayed in Figures 1 and 2, respectively. An example of the NO, NO<sub>2</sub>, and O<sub>3</sub> concentration–time profiles obtained in the absence of any surface using the outdoor chamber is shown in Figure S4.

Despite the different time scales and the chamber characteristics (i.e., irradiation type and chambers building material) the observed trace gas evolution is similar over a TiO<sub>2</sub> coated glass. In agreement with previous studies,<sup>26</sup> NO uptake on the TiO<sub>2</sub> coated glass is enhanced under irradiation increasing with time in both experiments. The NO<sub>2</sub> concentration profile exhibits a maximum under illumina-



**Figure 1.** NO, NO<sub>2</sub>, HNO<sub>2</sub>, and O<sub>3</sub> concentration profiles over (a) a TiO<sub>2</sub> coated glass and (b) a standard glass (TiO<sub>2</sub> free) in the CESAM chamber. The vertical line indicates the start of the irradiation.



**Figure 2.** NO, NO<sub>2</sub>, and O<sub>3</sub> profiles under natural irradiation in the presence of (a) a TiO<sub>2</sub> coated glass and (b) a standard glass in the outdoor chamber. The vertical line indicates the start of the irradiation.

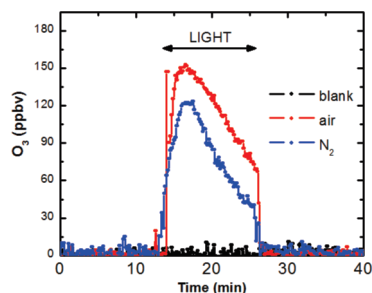
tion, suggesting that it is formed from NO photocatalytic oxidation and then converted into HNO<sub>3</sub> and HNO<sub>2</sub> at the surface.<sup>14–17,22</sup> At the same time, a significant accumulation of ozone is observed. In agreement with previous studies,<sup>14–16</sup> HNO<sub>2</sub> production is enhanced under irradiation in the presence of TiO<sub>2</sub> (Figure 1). However, when a standard glass (i.e., TiO<sub>2</sub> free) is analyzed in both chambers, no O<sub>3</sub> formation is observed (Figures 1b and 2b). The NO<sub>2</sub> and NO concentration–time profiles obtained in the absence of glass samples are similar to those observed in the presence of standard glasses, with no evidence of any light effect (Figures 2b and S4). These results clearly suggest that O<sub>3</sub> formation cannot be explained by the gas phase chemistry occurring in the chambers. The differences between the O<sub>3</sub> profiles from the blank experiments and the coated glass indicate that TiO<sub>2</sub> should be involved in the reaction mechanism leading to O<sub>3</sub> formation probably via new surface reactions.

To further investigate the reason for O<sub>3</sub> production, a second type of experiment has been carried out using a flow tube reactor, where only air or N<sub>2</sub> was present in the gas phase. It is well-known

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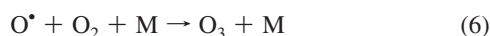
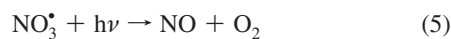
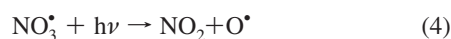
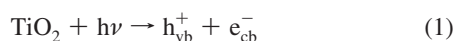
<sup>§</sup> ICARE.



**Figure 3.** Effect of light (8 near-UV emitting lamps in the 300–420 nm wavelength range) on a TiO<sub>2</sub>/KNO<sub>3</sub> (50% w/w) film using synthetic air and pure N<sub>2</sub> as carriers. The same blank signal was given by an empty tube and by a tube with a KNO<sub>3</sub> deposit using both carriers.

that nitrate anions are formed as a consequence of the photocatalytic oxidation of NO<sub>2</sub> on UV-illuminated TiO<sub>2</sub> surfaces.<sup>9,18–22</sup> Therefore a film of TiO<sub>2</sub>/KNO<sub>3</sub> 50% w/w has been exposed to near-UV irradiation (300–420 nm) using synthetic air or pure N<sub>2</sub> as a carrier gas with 30% RH under atmospheric pressure and at  $T = 298 \pm 1$  K (Figure 3).

As described previously, a renoxification process occurs on illuminated TiO<sub>2</sub> films mixed with nitrate.<sup>23</sup> In contrast with the mechanism proposed by Grassian and co-workers<sup>24,25</sup> for the photochemistry of adsorbed nitrate on alumina, control experiments indicate that nitrate photolysis is negligible under the experimental conditions (Figure 3). NO<sub>3</sub><sup>-</sup> reduction by conduction band electrons may lead to the release of NO<sub>x</sub>, but it does not explain O<sub>3</sub> formation.<sup>27</sup> An alternative surface chemical pathway would involve the photochemistry of the NO<sub>3</sub> radical, produced by a charge exchange reaction between the nitrate anion and the solid surface, followed by photolysis of the radical (occurring at longer wavelength compared to the anion)<sup>23</sup> according to



TiO<sub>2</sub> band gap excitation (eq 1) produces excited-state conduction-band electrons and valence-band holes, which can then react with electron acceptors and electron donors adsorbed onto the semiconductor surface. According to Marcus theory,<sup>28</sup> the activation energy ( $\Delta G^{\ddagger}$ ) for the oxidation of nitrate anion into nitrate radical by the holes can be calculated by eq 8:

$$\Delta G^{\ddagger} = \frac{\lambda}{4} \left( 1 - \frac{F(E_{\text{vb}} - E_{\text{NO}_3^{\bullet}/\text{NO}_3^-})}{\lambda} \right)^2 \quad (7)$$

where  $\lambda$  is the reorganization energy necessary to transform the nuclear configurations in the reactant and the solvent to those on the product state;  $E_{\text{vb}} = 3.25\text{--}0.06\text{pH V}$  (vs NHE) is the valence band edge potential<sup>29</sup> in TiO<sub>2</sub> and  $E = 2.3\text{--}2.5$  V (vs NHE) is the redox potential range for the NO<sub>3</sub><sup>•</sup>/NO<sub>3</sub><sup>-</sup> couple.<sup>30,31</sup> Assuming that the reorganization energy accounts for only the solvent contribution and that it is approximately 0.5 eV,<sup>29</sup> then  $\Delta G^{\ddagger}$  approaches zero, so  $h_{\text{vb}}^+$  can directly oxidize NO<sub>3</sub><sup>-</sup>.

New surface reactions occurring on illuminated TiO<sub>2</sub> surfaces are discussed, for the first time, as a possible source of O<sub>3</sub>. Although O<sub>3</sub> has been recently proven to decompose on illuminated TiO<sub>2</sub> surfaces,<sup>32</sup> its formation is observed when TiO<sub>2</sub> treated surfaces are exposed to NO<sub>x</sub> under illumination. Charge transfer reactions are taking place at the surface of TiO<sub>2</sub>, producing nitrate radicals from the corresponding anions. The photochemistry of the NO<sub>3</sub> radical leads to O<sub>3</sub> formation, enhancing the oxidizing power of these surfaces.

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**Supporting Information Available:** Experimental procedures, Figures S1–S4, and references. This material is available free of charge via the Internet at <http://pubs.acs.org>.

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